

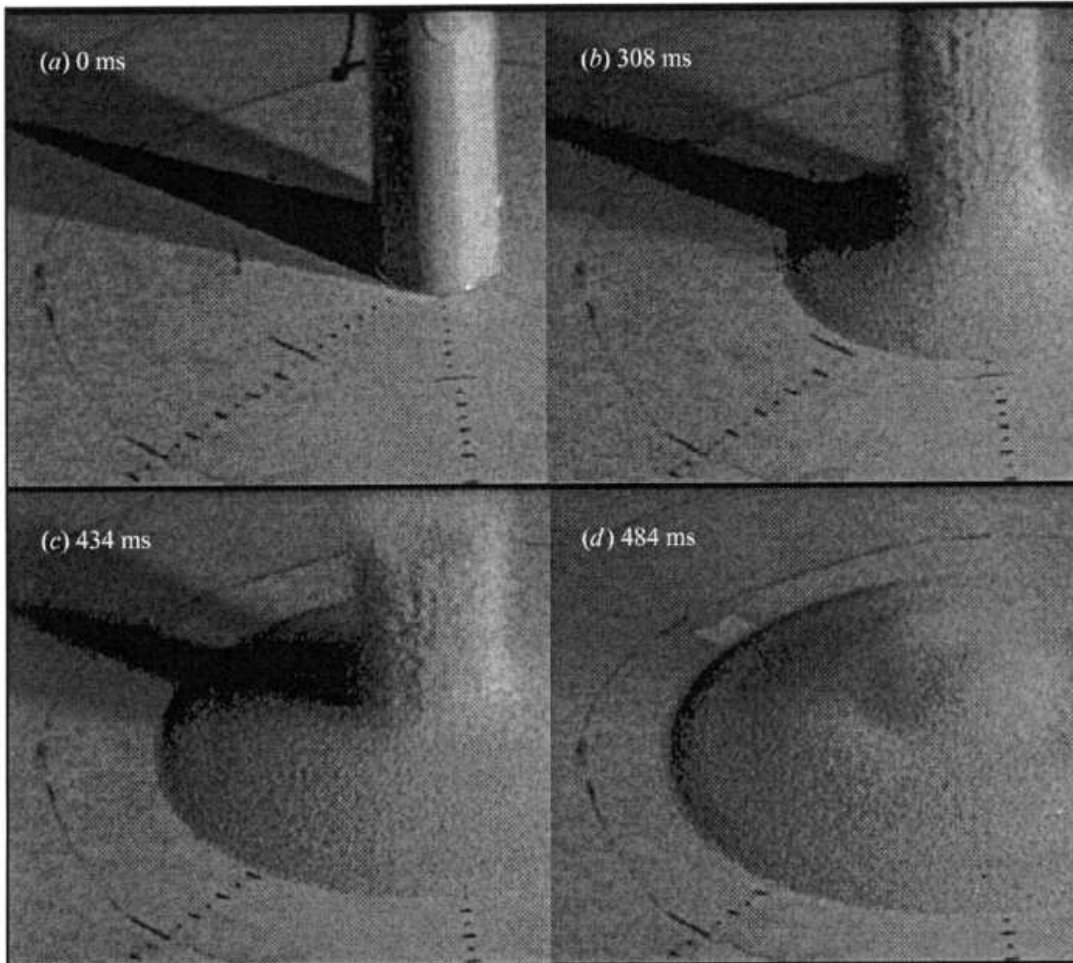
# **Collapse of a granular column**

John Hinch

in collaboration with Lydie Staron & Emeline Larrieu

inspired by Herbert Huppert

# Collapse of a granular column



Lube, Huppert, Sparks  
& Hallworth 2004 JFM

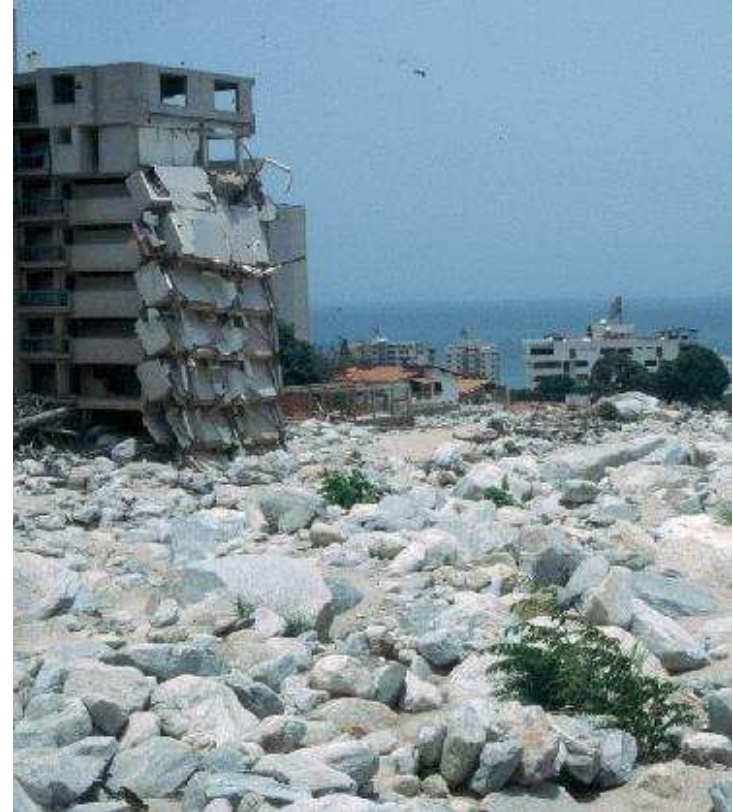
Idealisation of geophysical events

# Geophysical events



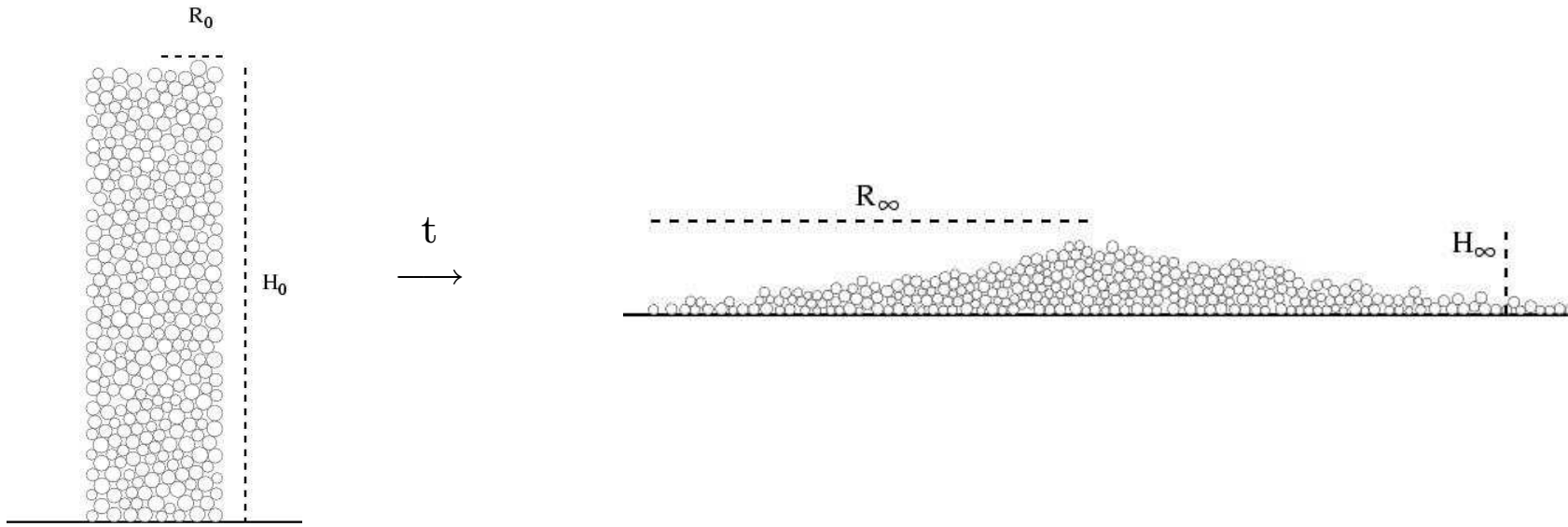
Hope, British Columbia, 1965

$4.6 \cdot 10^7 \text{ m}^3$



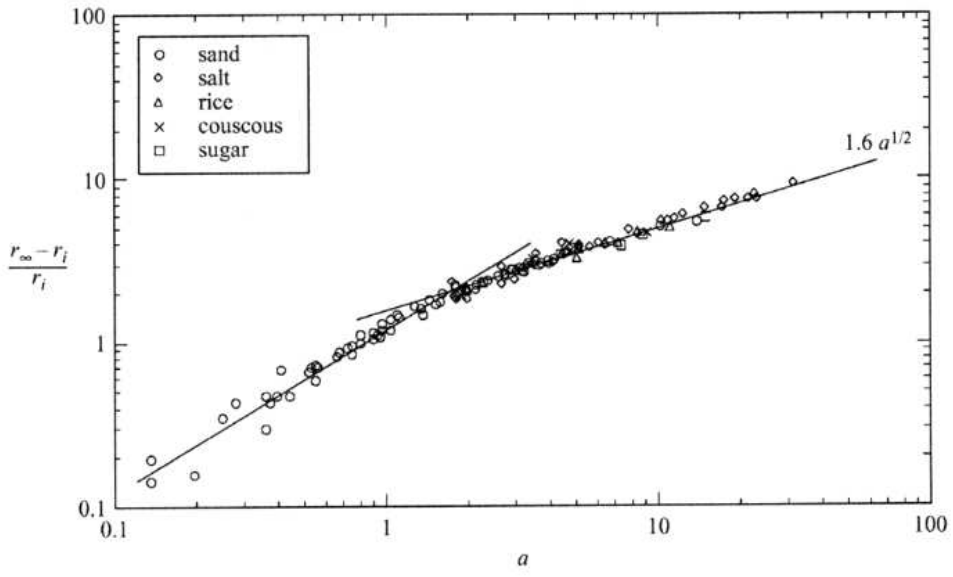
Venezuela

# Problem



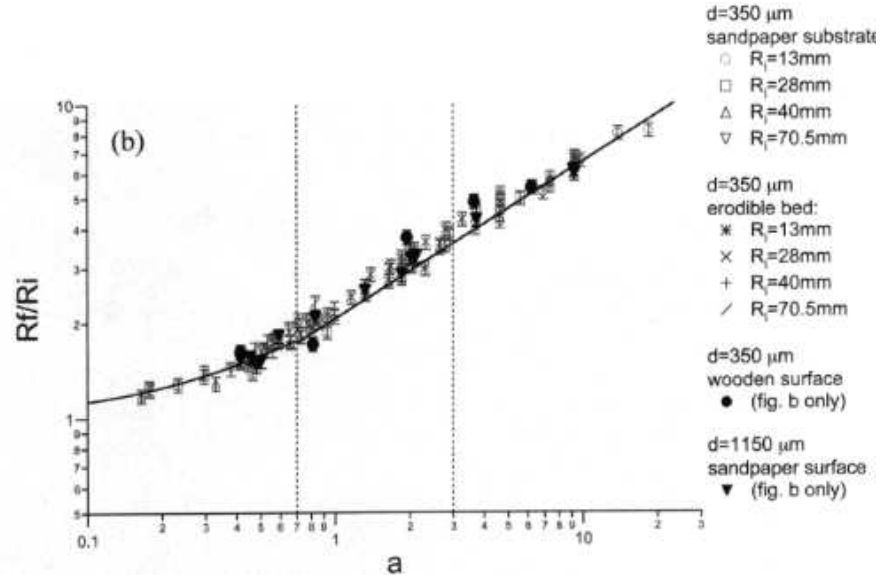
What determines the runout distance  $R_\infty$ ?

# Experiments

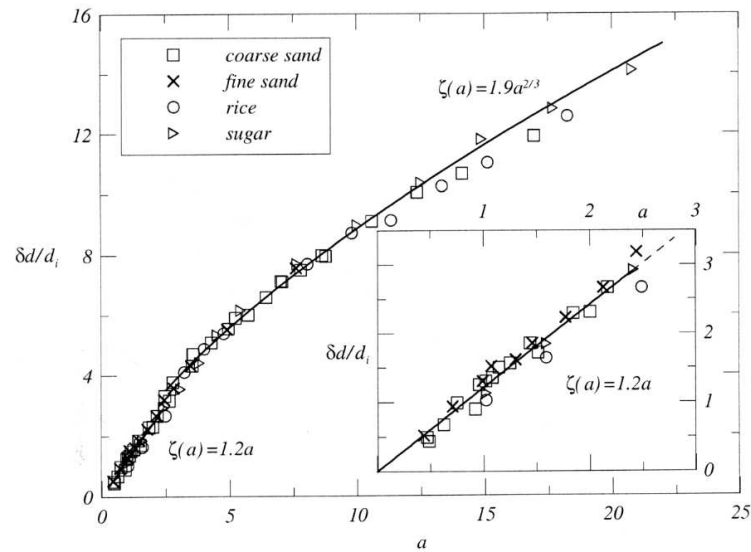


Lube, Huppert, Sparks & Hallworth 2004 JFM

Lajeunesse, Mangeney-Castelnau & Vilotte 2004 PoF

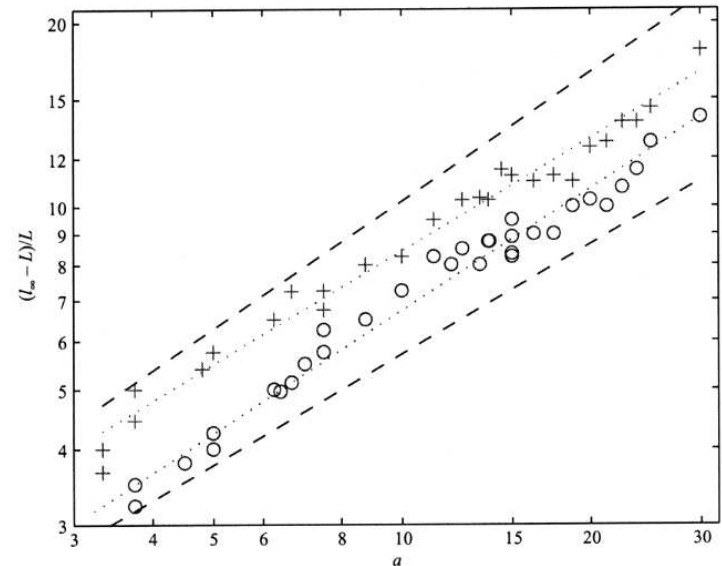


# Experiments in 2D channel



Lube, Huppert, Sparks  
& Freundt 2005 PRE

Balmforth & Kerswell  
2005 JFM





# Runout in experiments

By Huppert *et al*, by Lajeunesse *et al*, by Balmforth *et al*

Independent of type, size & number of particles

Axisymmetric:

$$R_{\infty}/R_0 = 1 + 1.8a^{1/2}$$

2D:

$$R_{\infty}/R_0 = 1 + 2a^{2/3}$$

if  $a > 2$ , where **aspect ratio**  $a = H_0/R_0$ .

Simple laws, difficult to explain

# Doomed theories

Initial potential energy  $\rho g H_0$

becomes vertical kinetic energy  $\frac{1}{2}\rho w^2 = \rho g H_0$

becomes horizontal kinetic energy  $\frac{1}{2}\rho u^2 = \frac{1}{2}\rho w^2$

Sliding mass  $M$  resisted by solid (Coulomb) friction  $\mu M g$

Runout:  $R_\infty = H_0/\mu$  **10× too large, wrong power-law**

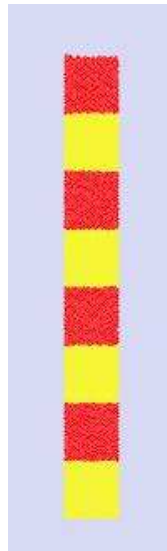


# Numerical simulations of grains flowing

1. **Event-driven:** for dilute granular gases, jump  $t$  to next collision, but condensate
2. **Soft-particle:** cannot resolve real deformation of 1 nm on 1  $\mu\text{s}$ , so artificially very soft, by  $10^{-6}$ , plus artificial dash-pots for dissipation
3. **Hard-particle:** repulsive force to stop overlap, Coulombic friction in sliding contacts, underdetermined

# Numerical simulations by Lydie

DEM method, 2D, hard spheres (discs),  
Coulombic friction, 5000 particles, polydisperse sizes.



# Robust numerical simulations

Results independent of

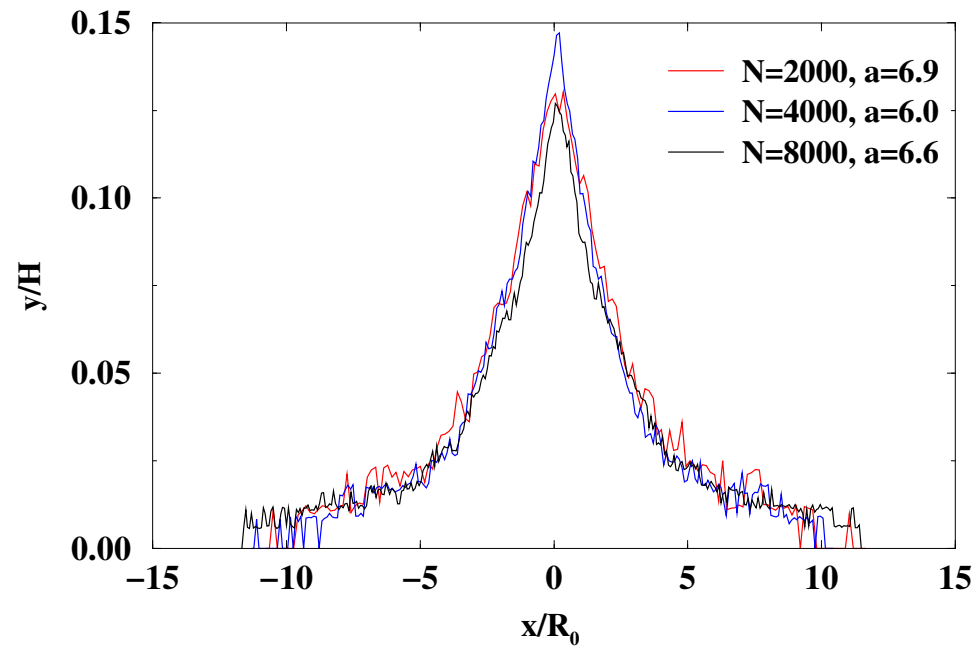
- number of particles
- polydispersity in size of particles
- value of coefficient of Coulombic friction
- value of coefficient of restitution

except for extreme cases.

Consider final deposits for different parameters

# Independent of number of grains

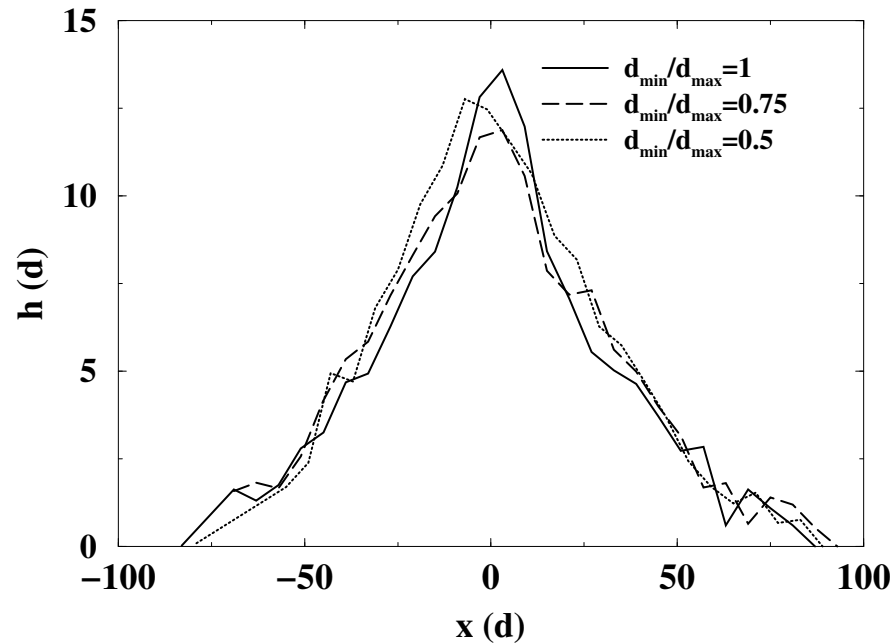
Final deposit:



# Independent of polydispersity

Uniform distribution of radii between in  $[d_{\min}, d_{\max}]$ ,  
with  $d_{\min}/d_{\max} = 1, 0.75, 0.5$

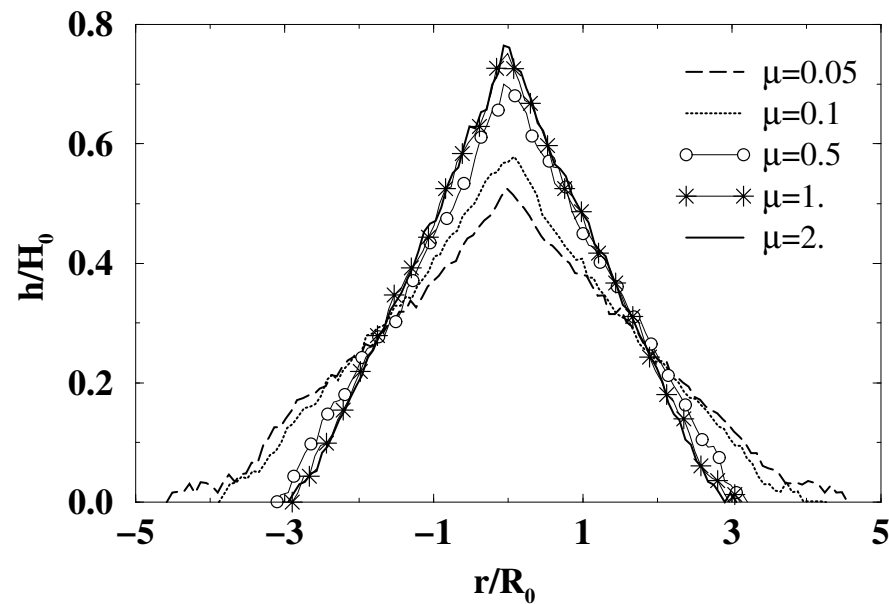
Final deposit:



Small fines would segregate and fall to bottom

# Independent of inter-grain friction

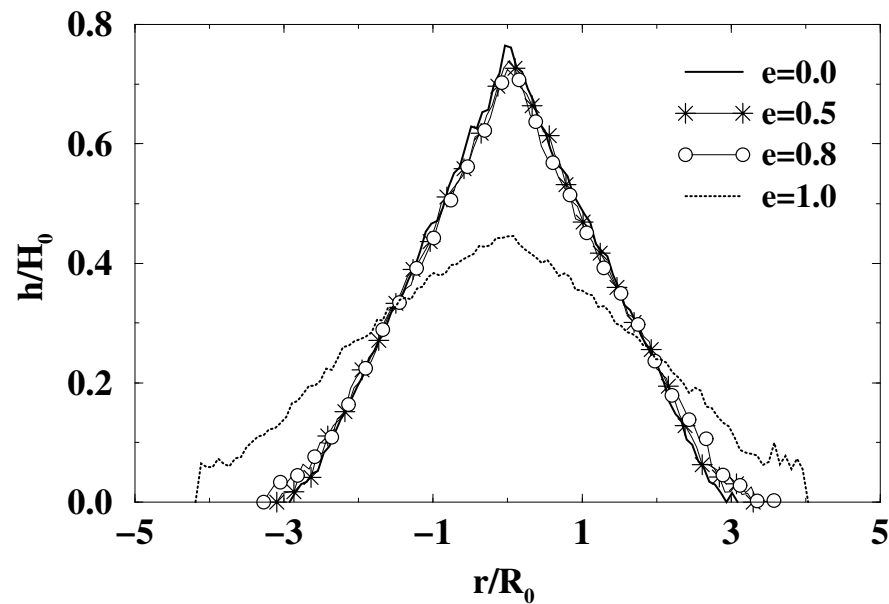
Final deposit for  $\mu = 0.05, 0.1, 0.5, 1, 2$



Different only if very slippery

# Independent of restitution

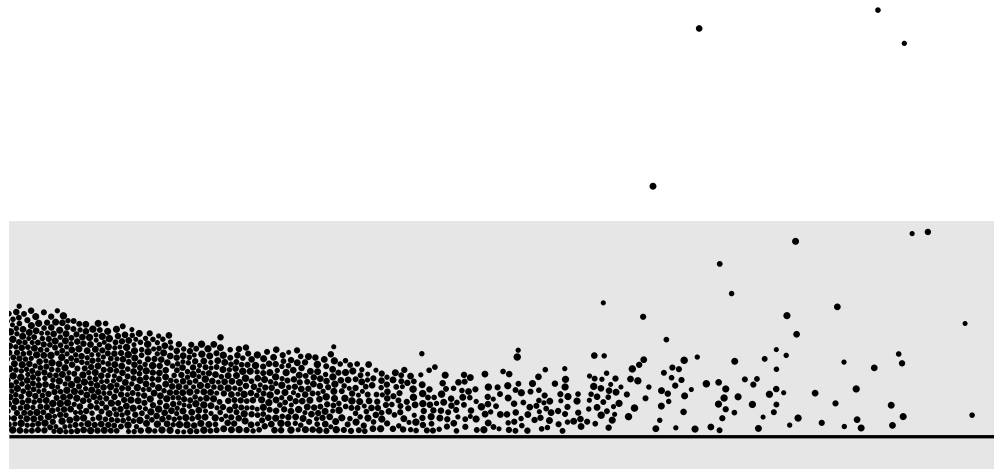
Final deposit for  $e = 0, 0.5, 0.8, 1.0$



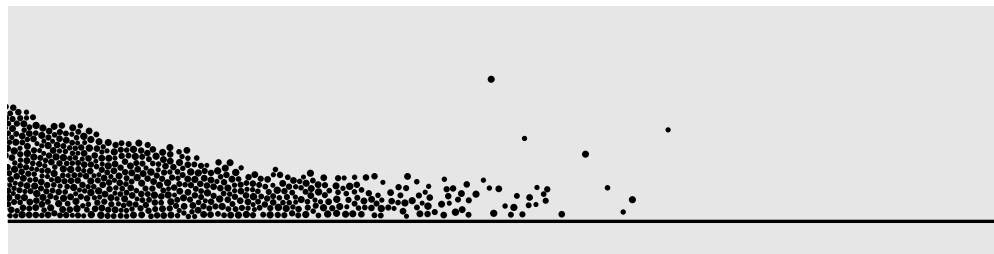
Different only if  $e$  very close to 1



# Effect of restitution



$e = 1.0$



$e = 0.8$

Too bouncy if  $e = 1$ .

# Numerical simulations

Results independent of

- number of particles
- polydispersity in size of particles
- value of coefficient of Coulombic friction
- value of coefficient of restitution

except for extreme cases.

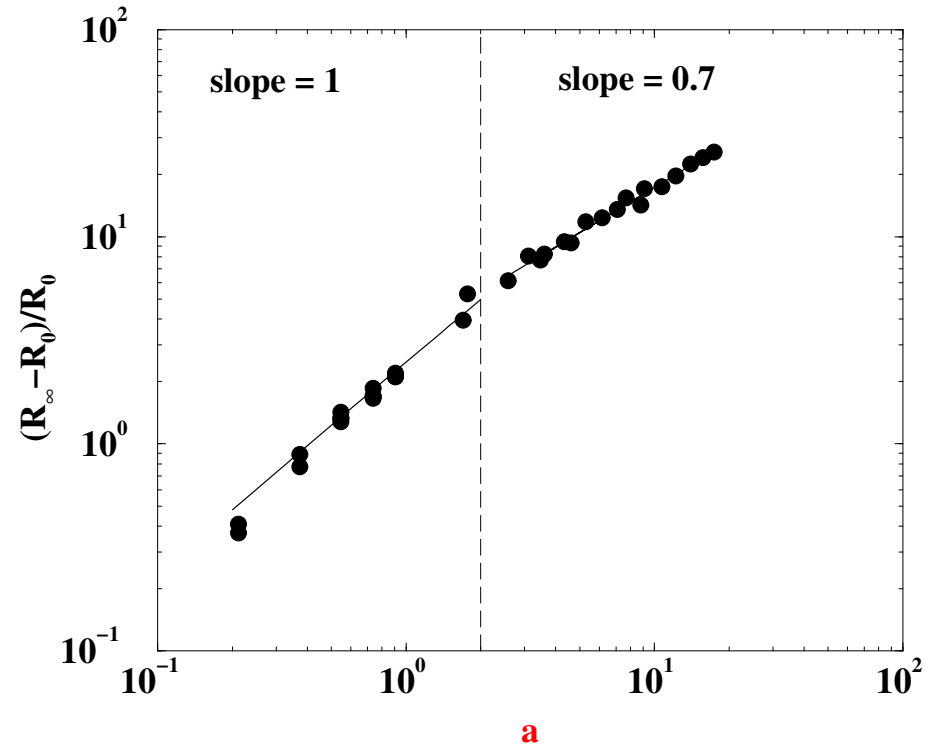
Like independent of type, size & number of particles in experiments.

# Results of simulations

Runout (in 2D):

If  $a > 2$

$$R_{\infty}/R_0 = 1 + 3.5a^{0.7}$$



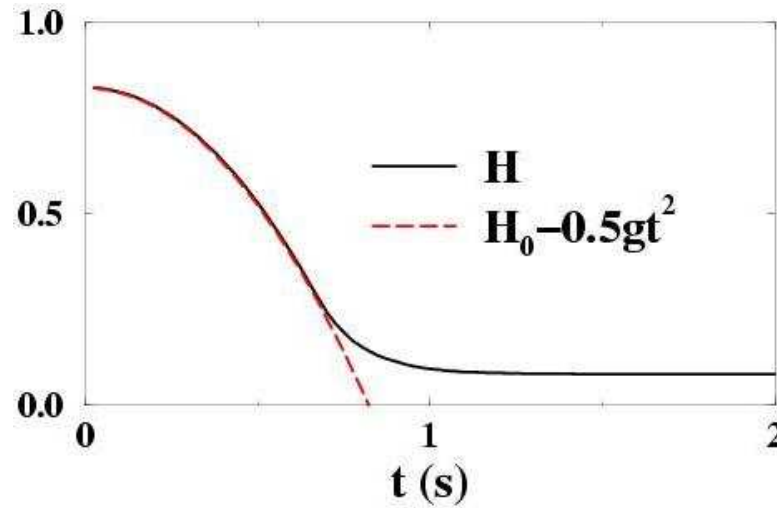
Simulations 3.5 vs experiments 2.

Dissipation low for discs?

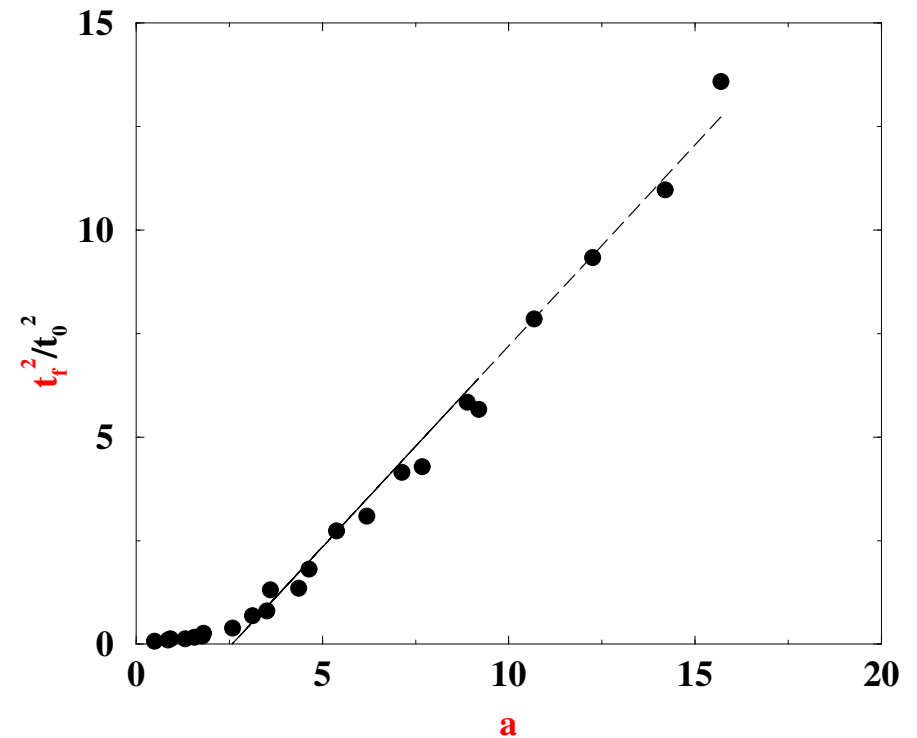
# ... more details

- Free fall of column while  $h(t) > 2.5R_0$
- Duration of flow  $T_\infty = 2.25\sqrt{2H_0/g}$
- Universal position of front as function of time, normalised
- Dissipation in horizontal flow

# Free fall

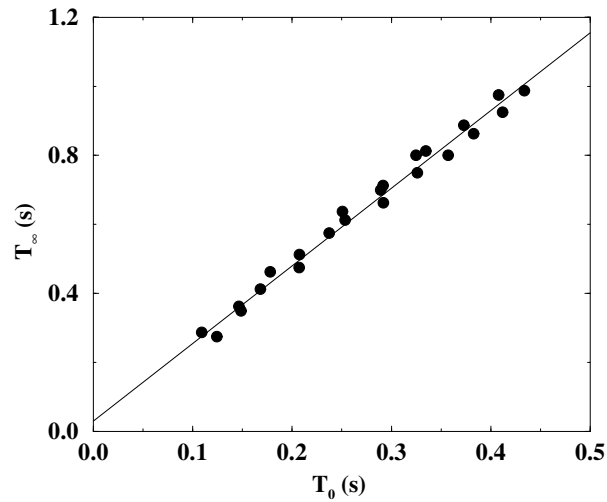


Column in free fall for  
 $t_f = \sqrt{2(H_0 - 2.5R_0)/g}$



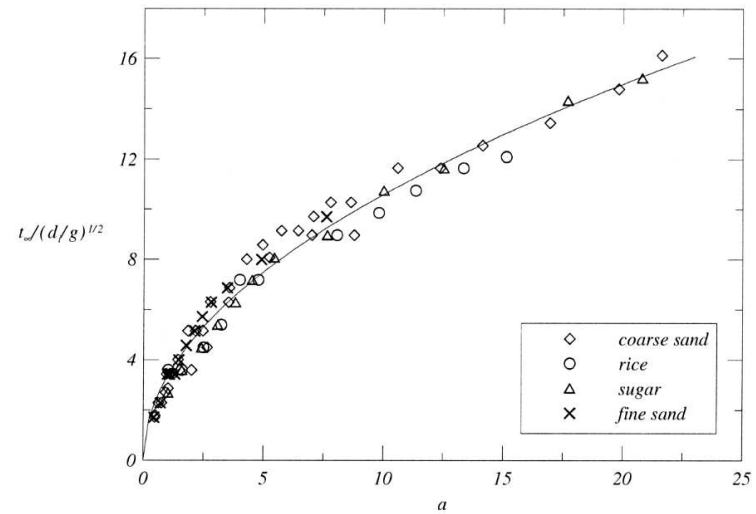
# Duration of flow, $T_\infty$

## Simulations



$$T_\infty = 3.2\sqrt{H_0/g}$$

## Experiments



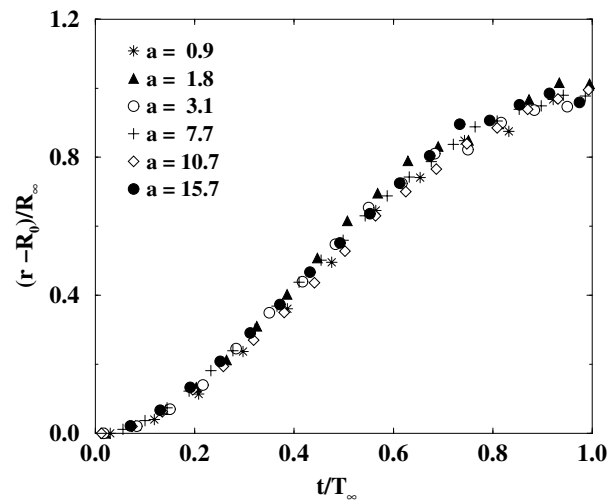
Lube, Huppert, Sparks & Freundt 2005 PRE

$$T_\infty = 3.3\sqrt{H_0/g}$$

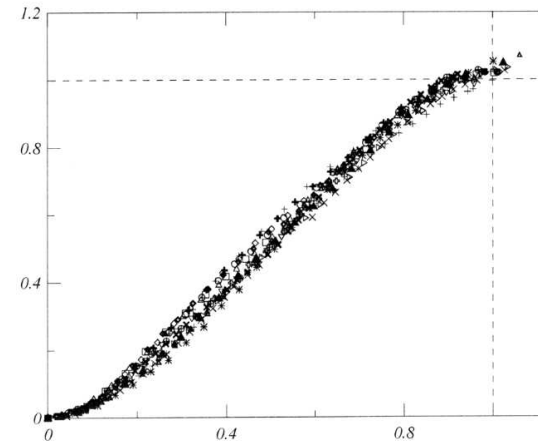
# Moving front

Front  $r(t)$ :  $(r - R_0)/R_\infty$  vs  $t/T_\infty$

## Simulations



## Experiments

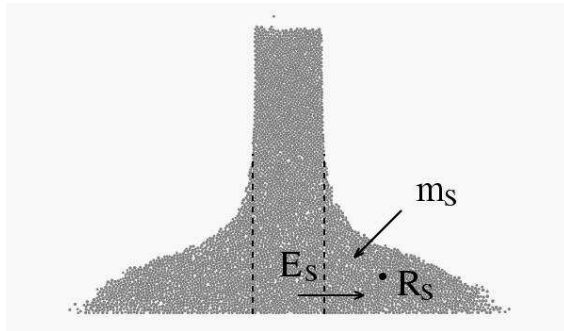


Lube, Huppert, Sparks & Freundt 2005 PRE

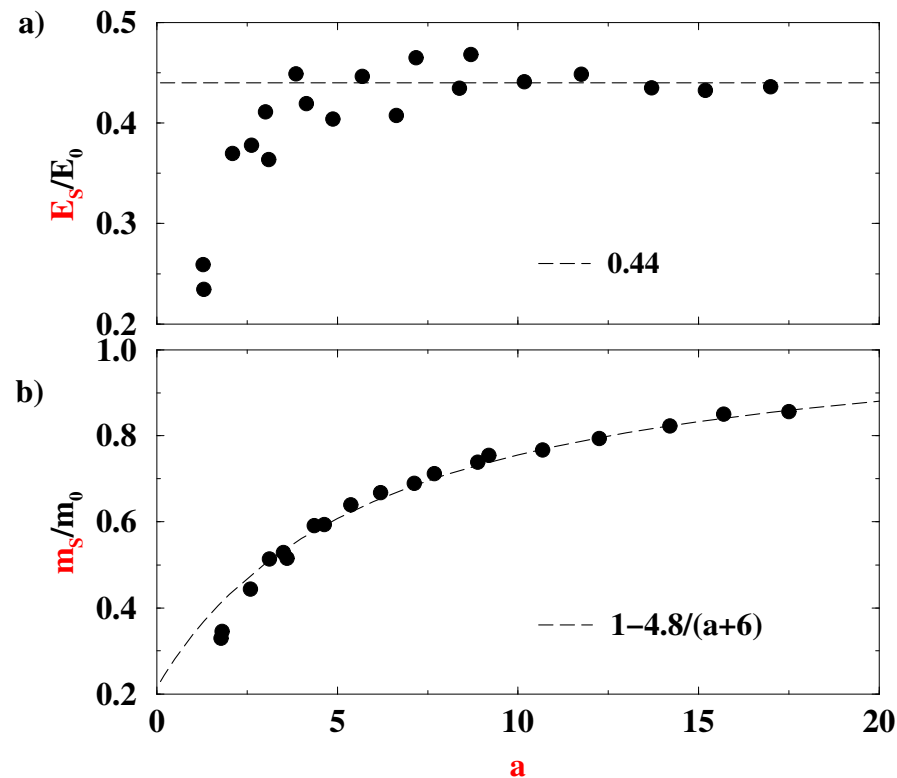
Intermediate times at nearly constant velocity  $\sqrt{2gR_0}$



# The horizontal flow

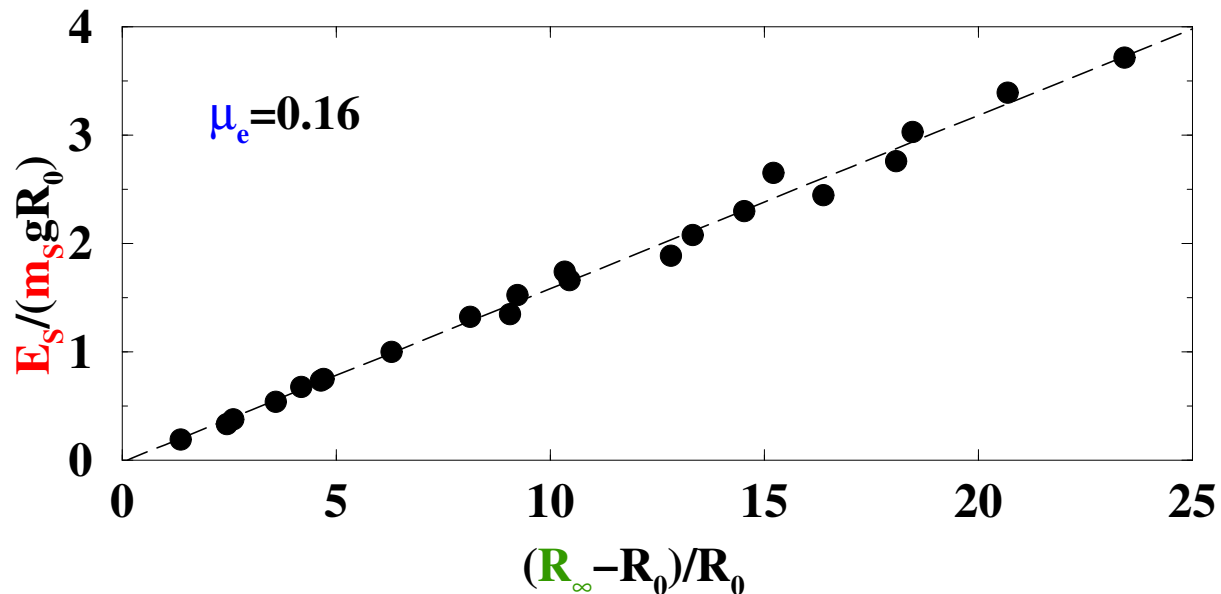


Mass flowing  $m_s$  and associated energy  $E_s$  as function of aspect ratio  $a$



# Dissipation of horizontal flow

Flowing mass  $m_S$  with energy  $E_S$  has runout  $R_\infty$



$$E_S = \mu_e m_S g (R_\infty - R_0)$$

with simple effective friction  $\mu_e = 0.16$  independent of  $a$ .

$\mu_e = 0.47$  for centre of mass

# A shallow-water model

For runout in a thin layer

Depth-averaged horizontal velocity  $\bar{u}$

Depth-integrated horizontal momentum:

$$\frac{\partial(h\bar{u})}{\partial t} + \beta \frac{\partial(h\bar{u}^2)}{\partial r} = -Kgh \frac{\partial h}{\partial r} - \mu gh$$

with

- $\beta$  velocity profile factor
- $K$  'Earth coefficient'
- $\mu$  basal Coulomb friction coefficient

# Velocity profile factor $\beta$

Mass flux to momentum flux correction:

$$\beta = h \int_0^h u^2 dz / \left( \int_0^h u dz \right)^2$$

value depends on velocity profile in vertical

$$\beta = \begin{cases} 1 & \text{plug-flow} \\ \frac{4}{3} & \text{linear} \\ \frac{6}{5} & \text{parabolic} \end{cases}$$

# Earth coefficient $K$

‘Hydrostatic’ balance in vertical

$$\sigma_{zz} = -\rho g(h(x) - z)$$

Plastic yielding

$$\sigma_{xx} = K \sigma_{zz} \quad \text{with} \quad K = \frac{1 + \sin \delta}{1 - \sin \delta}$$

Horizontal ‘pressure gradient’

$$\frac{\partial \sigma_{xx}}{\partial x} = -K \rho \frac{\partial h}{\partial x}$$

Now

$$K = \begin{cases} 1/3 & \text{in ‘passive failure’} & u_x > 0 \\ 3 & \text{in ‘active failure’} & u_x < 0 \end{cases}$$

BUT best  $K = 1$

Pouliquen & Forterre 2002 JFM

# Basal friction $\mu$

Take  $\mu = 0.43$  to fit runout in simulations.

$$\frac{\partial(h\bar{u})}{\partial t} + \beta \frac{\partial(h\bar{u}^2)}{\partial r} = -Kgh \frac{\partial h}{\partial r} - \mu gh$$

Also take  $\beta = 1$  for simplicity, and  $K = 1$  as in previous studies.

Speculate: no change in qualitative behaviour for different values of coefficients

# 'Raining' into shallow water

Initial tall column is not shallow,  
but known to free-fall, so velocity at base is  $gt$

Add **mass** to thin horizontal layer as **rain** from the tall column

$$\frac{\partial h}{\partial t} + \frac{\partial(\bar{u}h)}{\partial r} = q$$

where

$$q(r, t) = \begin{cases} gt & 0 \leq r \leq R_0 \\ 0 & R_0 < r \end{cases} \quad \text{for } 0 < t < \sqrt{2H_0/g}$$

No change to momentum equation, as adding mass with zero horizontal momentum.

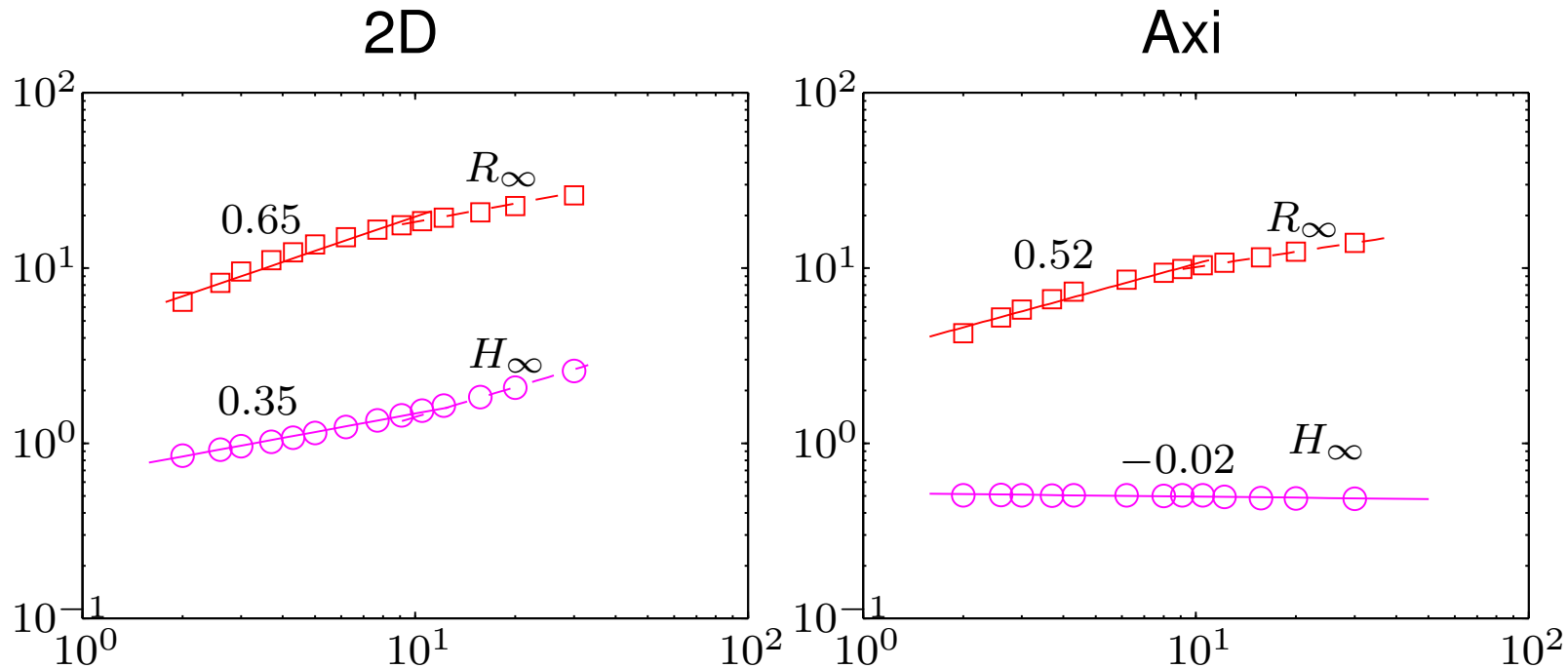


# Numerical method

- Conservative, shock-capturing, Roe solver
- Pre-layer  $10^{-7}$ , initial column height  $10^{-1}$
- Validation: dam-break ( $\mu = 0$ ) in 2D
- Alternative Lagrangian method for 2D

# Results from shallow-water model

## Runout

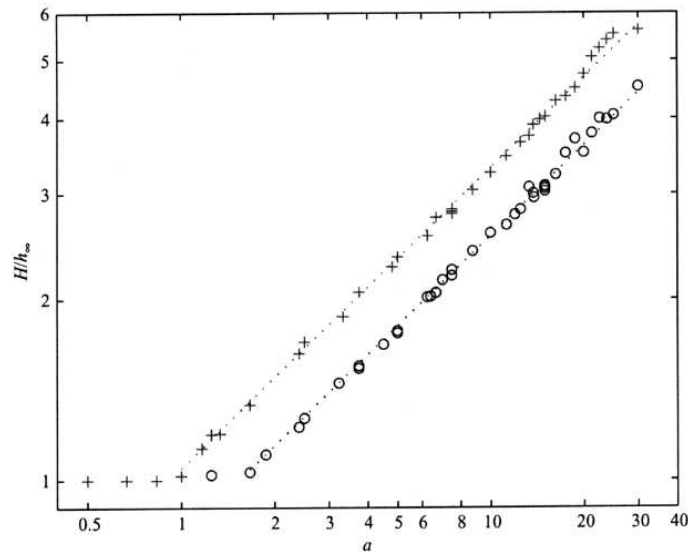


$$R_\infty/R_0 = \begin{cases} 1 + 4.4a^{0.65} & \text{2D} & 4.4 \longrightarrow 2 \text{ in experiments} \\ 1 + 3.2a^{0.52} & \text{Axi} & 3.2 \longrightarrow 1.8 \text{ in experiments} \end{cases}$$

# Height of deposit

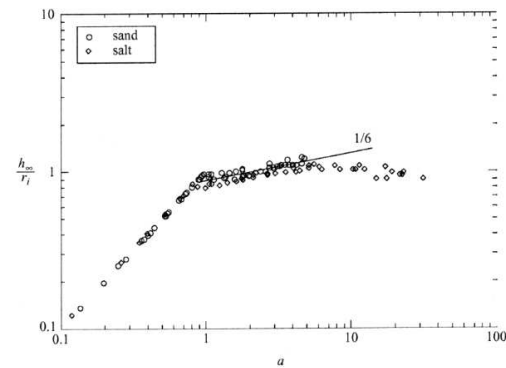
$$H_{\infty}/R_0 = \begin{cases} 0.66a^{0.35} & \text{2D} & 0.66 \longrightarrow 1 & \text{in experiments} \\ 0.52a^{-0.02} & \text{Axi} & 0.52 \longrightarrow 1 & \text{in experiments} \end{cases}$$

2D

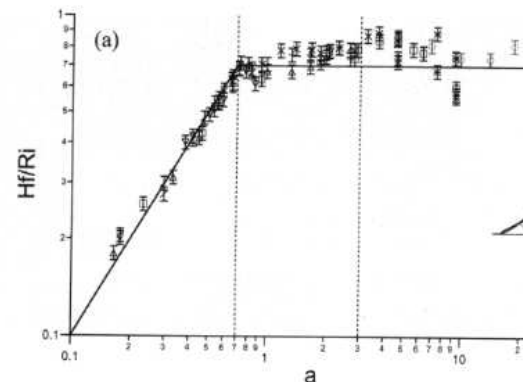


Balmforth & Kerswell 2005 JFM

Axi



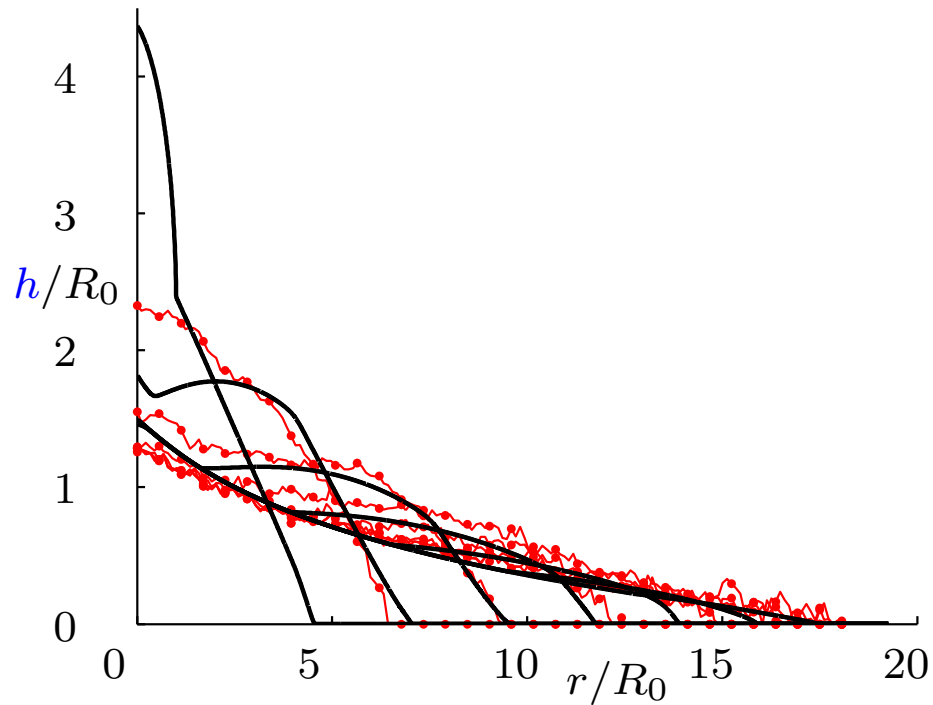
Lube, Huppert, Sparks & Hallworth 2004 JFM



Lajeunesse, Mangeney-Castelnau & Vilotte  
2004 PoF

# Evolution of deposit

Shallow-water vs Simulations

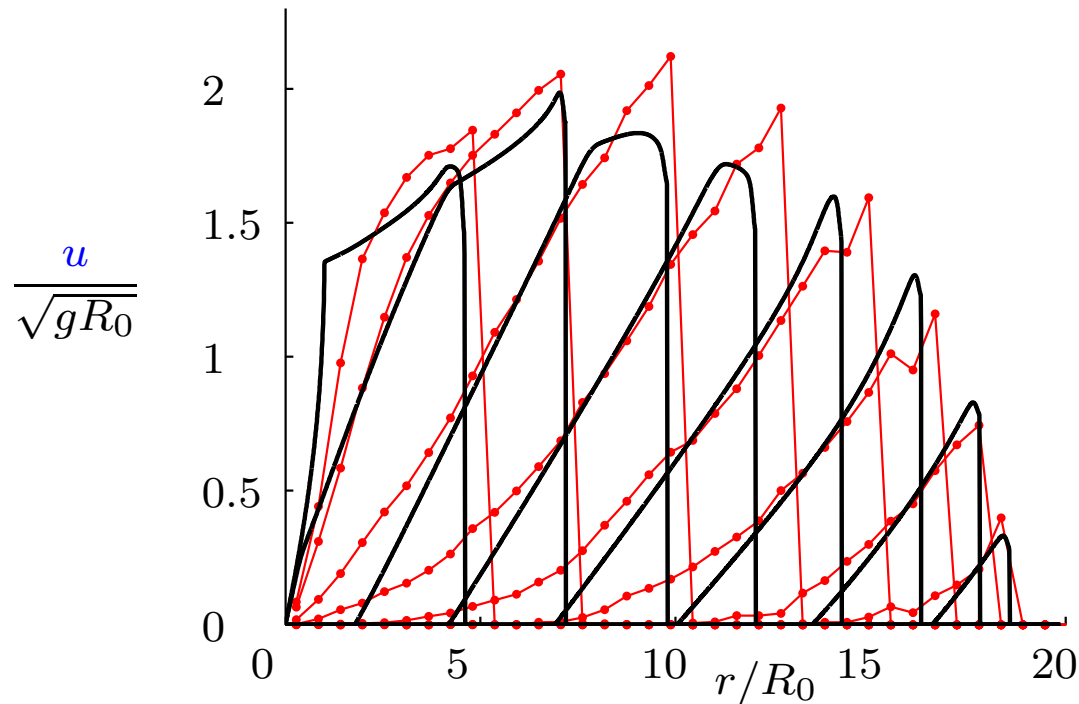


i

$$t = 0.3 (0.1) 0.9, \quad a = 9.1$$

# Velocity profiles

Shallow-water vs Simulations



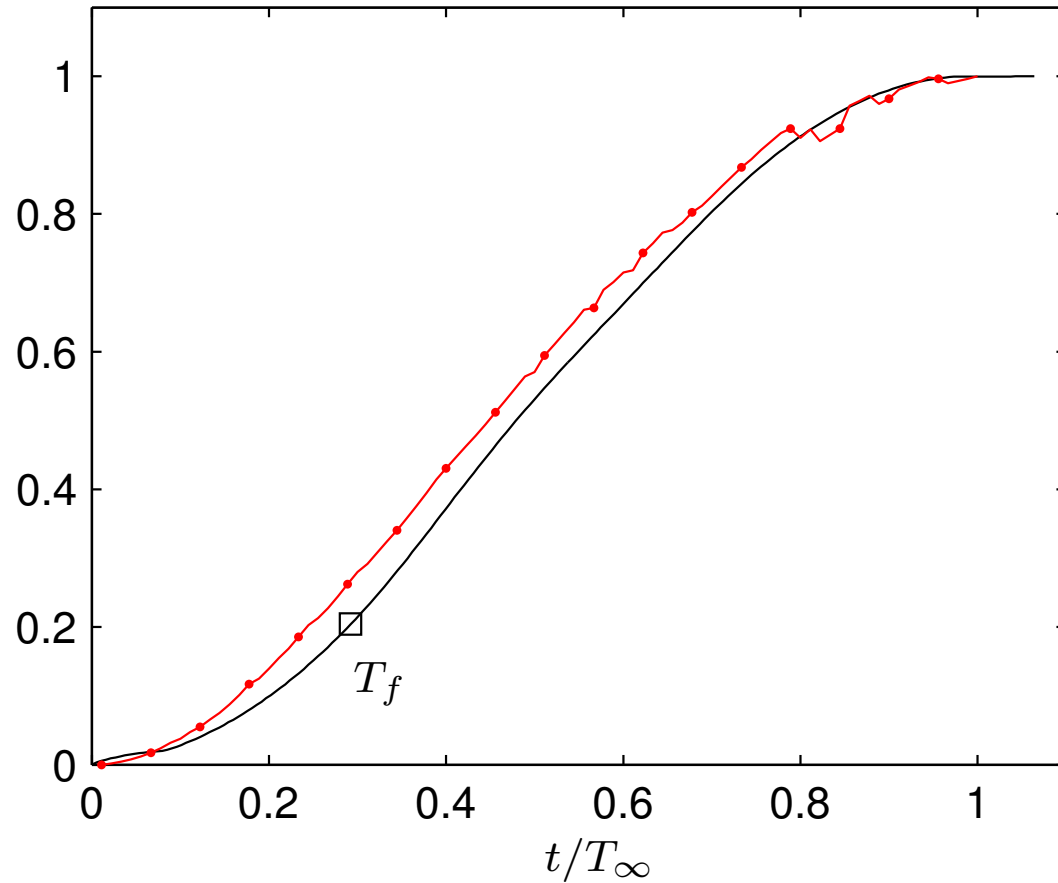
$$t = 0.4 \ (0.1) \ 0.9, \ a = 9.1$$

Stops from the centre, triangle wave propagates

# Moving front

Shallow-water vs Simulations

$$\frac{r(t) - R_0}{R_\infty - R_0}$$



# A little explanation?

Why 2D different from axisymmetric?

Simple power-laws?

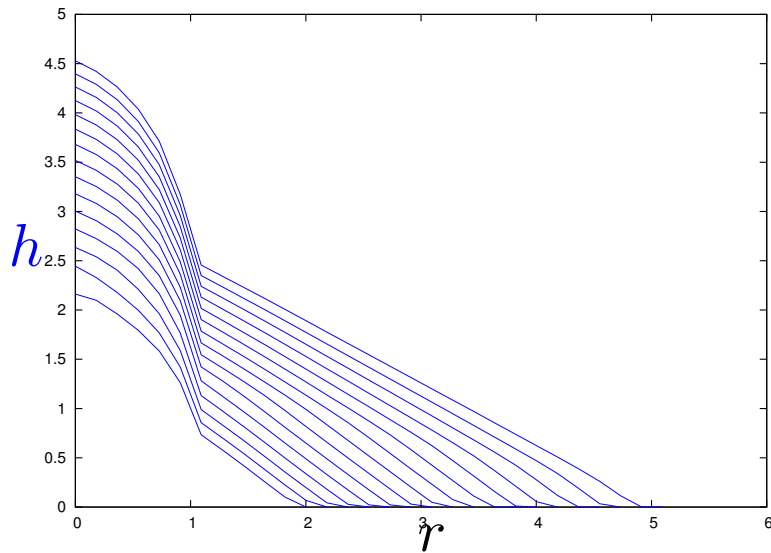
Three phases

- Leaving the base
- Propagating wave
- Deceleration

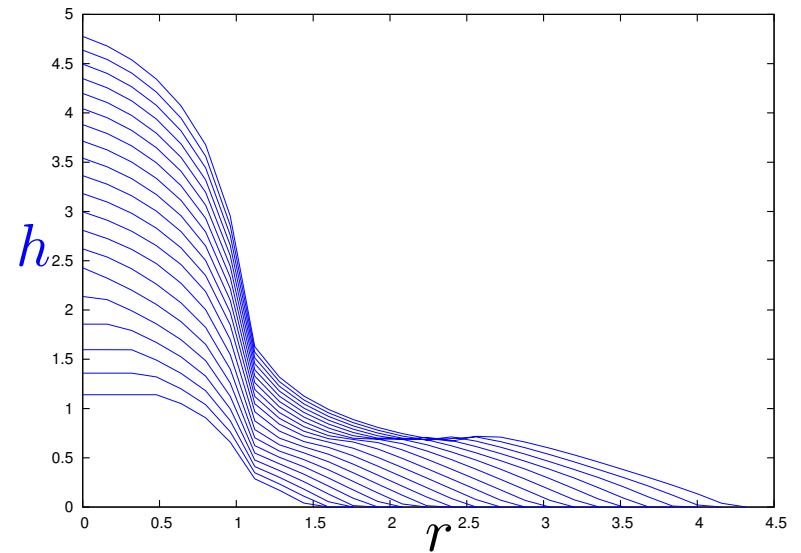
# Leaving the base

During the rain  $1.5 < t < 4.2 = \sqrt{2a}$ ,  $a = 9.1$

2D



Axi

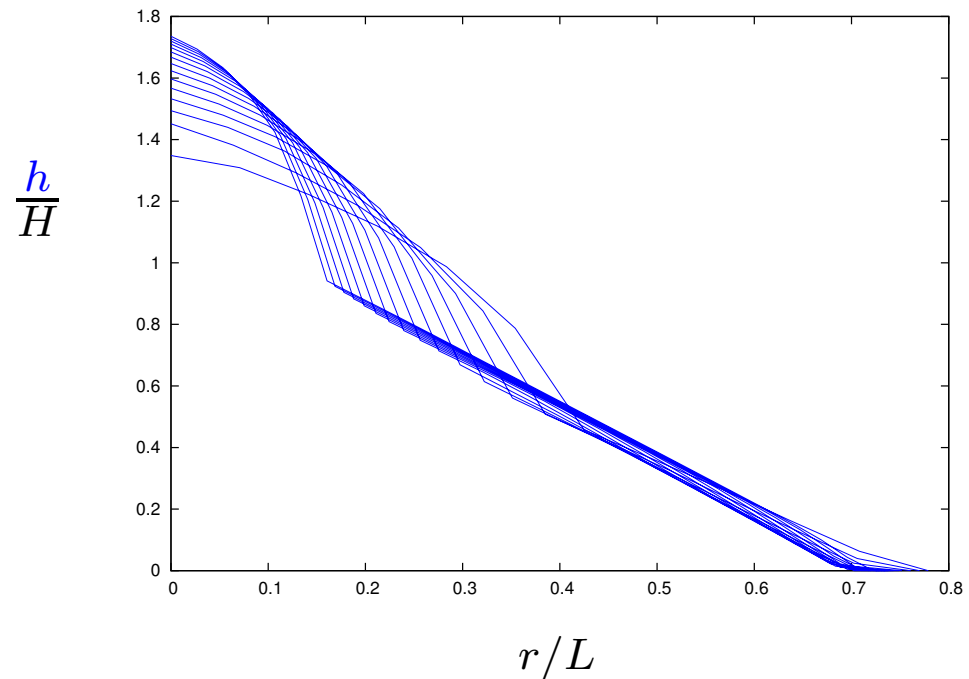




# Leaving the base of the column, 2D

- Height  $H(t)$  length  $L(t)$
- Mass in 2D :  $HL = gt^2 R_0$
- Acceleration by slope:  $L/t^2 = gH/L$

$$L(t) = (gt^2)^{2/3} R_0^{1/3}$$
$$H(t) = (gt^2)^{1/3} R_0^{2/3}$$

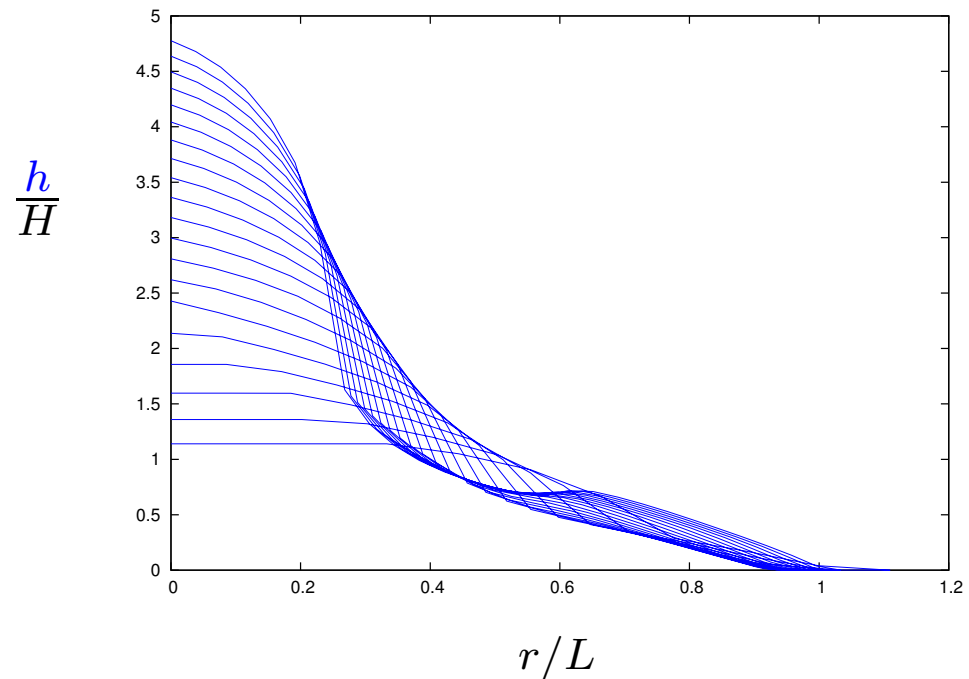


At the end of the rain  $L = 1.1R_0 a^{2/3}$

# Leaving the base of the column, Axi

- Height  $H(t)$  et Length  $L(t)$
- Mass in Axi :  $HL^2 = gt^2 R_0^2$
- Acceleration by slope:  $L/t^2 = gH/L$

$$L(t) = (gt^2)^{1/2} R_0^{1/2}$$
$$H(t) = R_0$$



At the end of the rain  $L = 1.4R_0 a^{1/2}$

# Difference between 2D and Axi

Axisymmetric geometry has more area to store grains, so shorter runout and lower height

$$L = \begin{cases} 1.4a^{1/2} & \text{Axi} \\ 1.1a^{2/3} & \text{2D} \end{cases}$$

at the end of the rain  $t = \sqrt{2gH_0}$ .

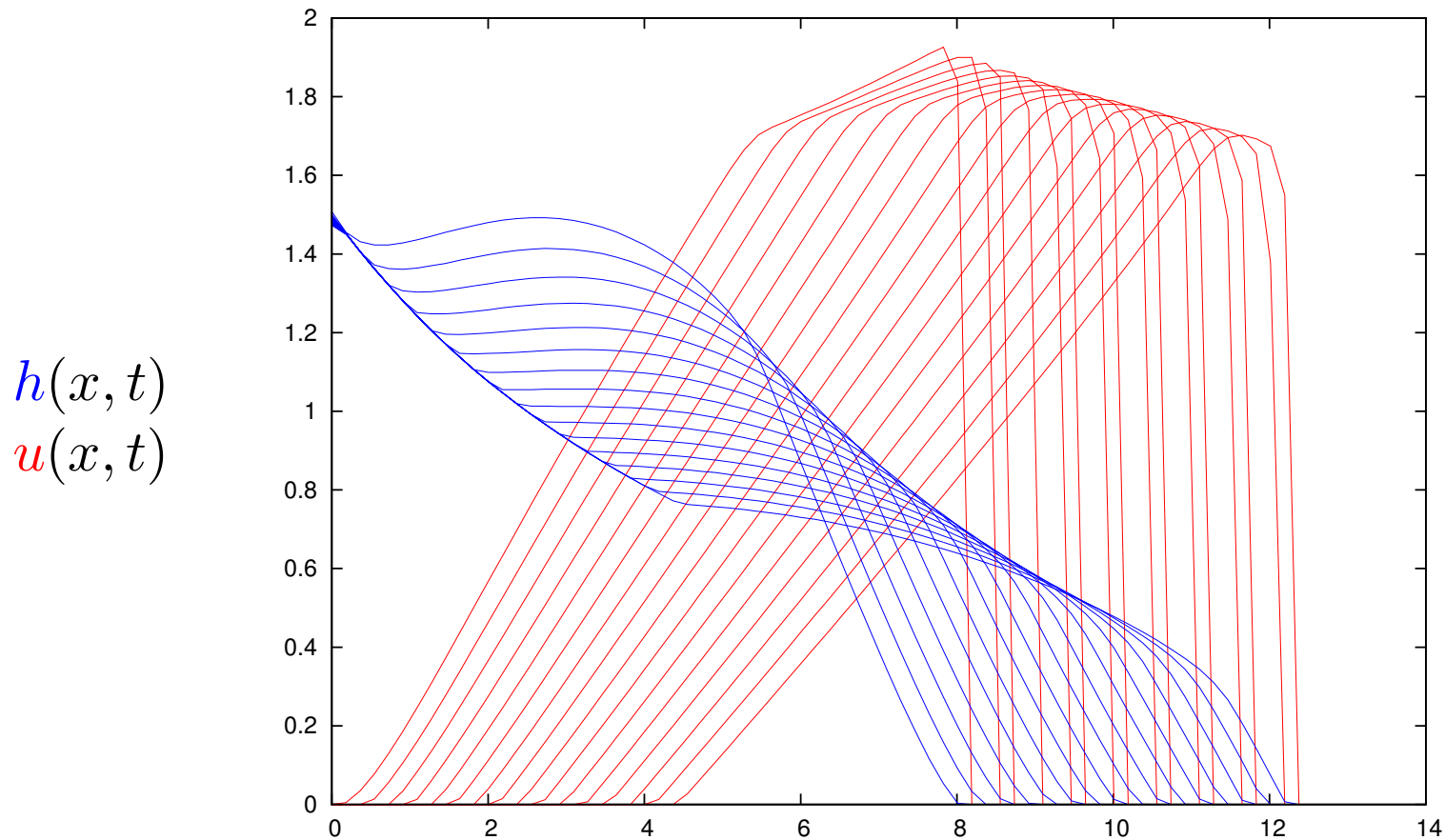
Final runout c3 times greater, but moving at  $2\sqrt{gR_0}$ .

However deceleration of  $2\sqrt{gR_0}$  at  $\mu g$  would only double runout.  
Need further.

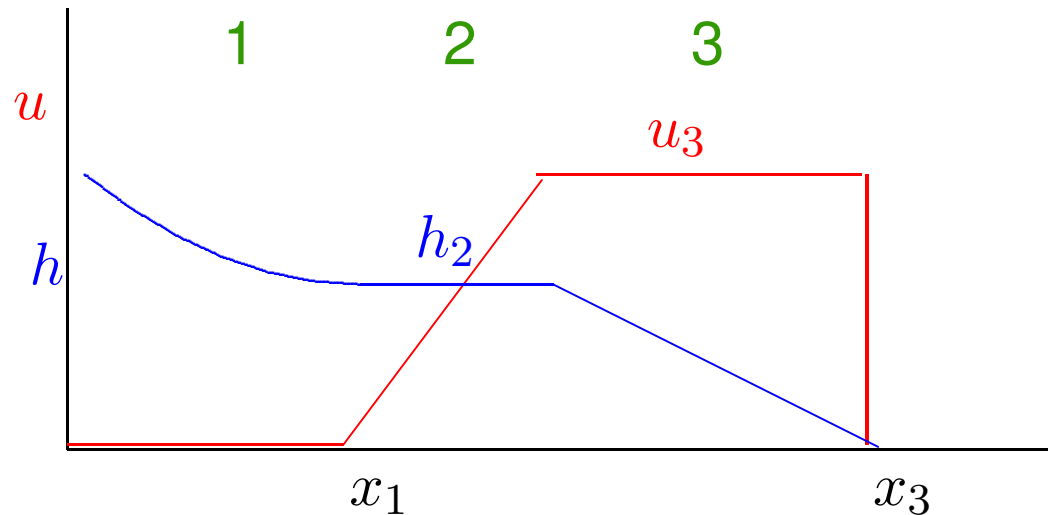
# Propagation of a wave, 2D

Extends runout before deceleration.

$$5.8 < t < 8.1, \quad a = 9.1$$



# A trapezoidal wave?



**1: stopped**  $u(x, t) = 0, \quad h(x, t) = h(x, \infty)$

**2: flat**  $h(x, t) = h_2(t), \quad u(x, t) = \alpha(t)(x - x_1(t))$

**3: constant velocity**  $u(x, t) = u_3,$

at angle of repose  $h(x, t) = \mu(x_3(t) - x)$

## Region 2

Flat  $h(x, t) = h_2(t)$ , so decelerate with  $\mu g$

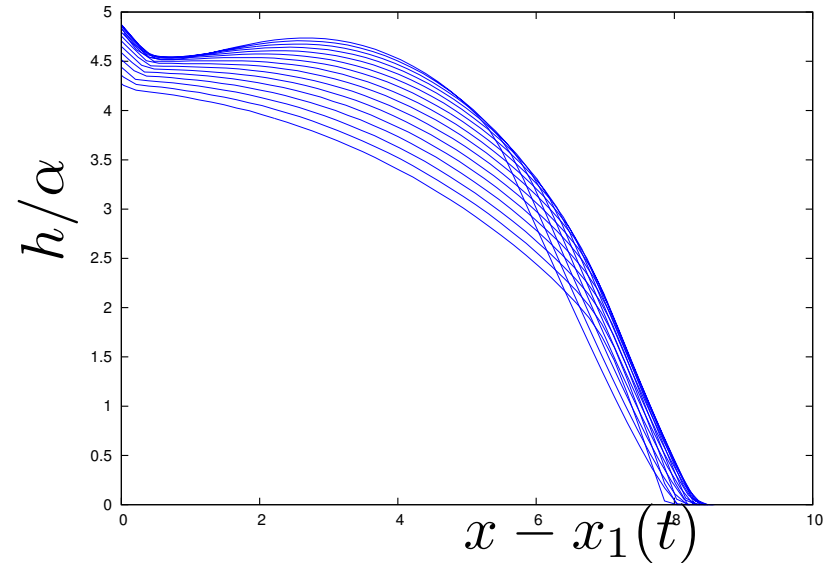
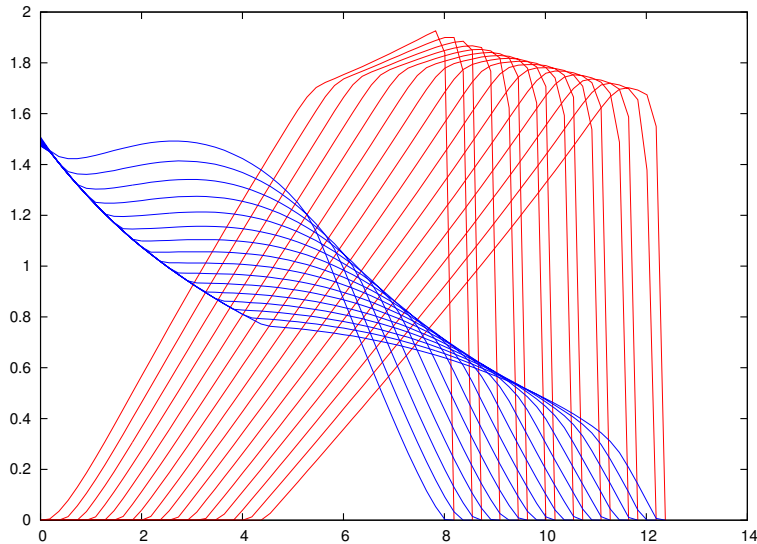
Linear velocity  $u(x, t) = \alpha(x - x_1)$  is constant deceleration if

$$\alpha(t) = \frac{1}{t - t_0} \quad \text{and} \quad x_1(t) = x_0 + \frac{1}{2}\mu g(t - t_0)^2$$

And height decrease as  $h_2(t) = h_0\alpha(t)$

Test by plotting  $h(x, t)/\alpha$  and  $u(x, t)/\alpha$  vs  $x - x_1$

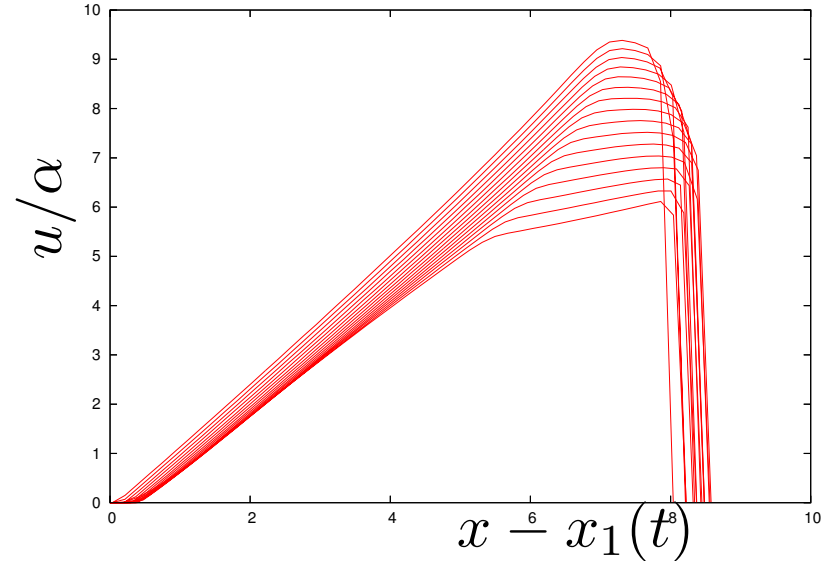
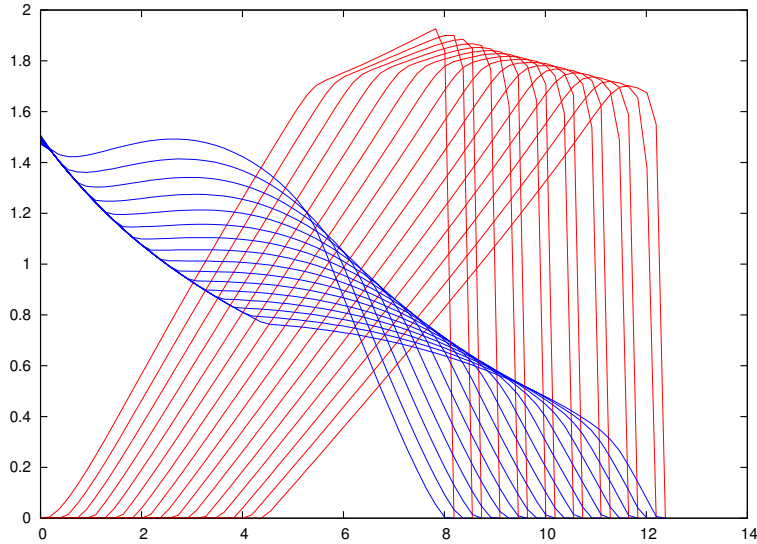
# Test solution for $h$ in region 2



$$\alpha(t) = \frac{1}{t - t_0} \quad \text{and} \quad x_1(t) = x_0 + \frac{1}{2}\mu g(t - t_0)^2$$

Deceleration at  $\mu g$

# Test solution for $u$ in region 2



$$\alpha(t) = \frac{1}{t - t_0} \quad \text{and} \quad x_1(t) = x_0 + \frac{1}{2}\mu g(t - t_0)^2$$

Deceleration at  $\mu g$



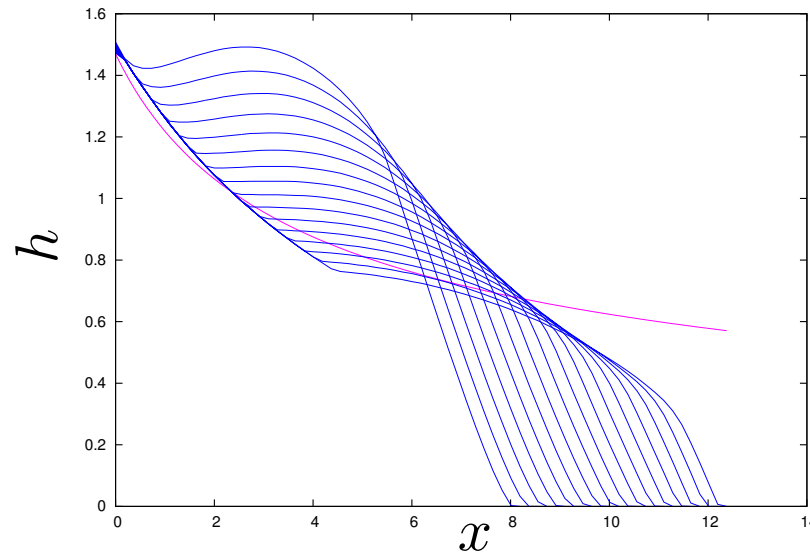
# Shape of final deposit, region 1

Final deposit

$$h(x, \infty) = h_2(t) \quad \text{at} \quad x = x_1(t)$$

So

$$h(x, \infty) = \frac{h_0}{\sqrt{2(x - x_0)/\mu}}$$



# Extension of runout during wave propagation

Initial length  $L = 1.1R_0 a^{2/3}$  of region 3 where  $u = u_3 = 2\sqrt{gR_0} a^{1/6}$

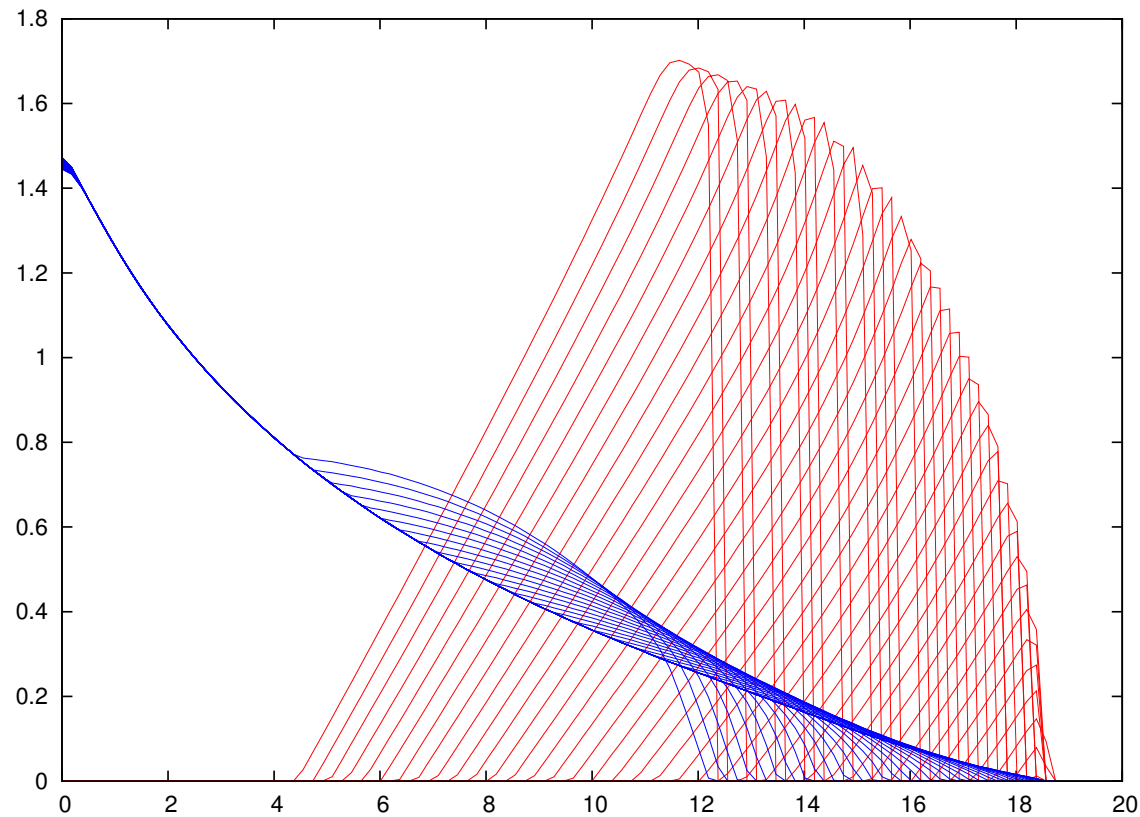
Accelerate at  $\mu g$  through  $L$  in time  $\sqrt{\frac{2L}{\mu g}}$

Distance travelled at  $u_3$  is  $2.2R_0 a^{1/2}$

# Deceleration, 2D

$8.3 < t < 14$ ,  $a = 9.1$

$h(x, t)$   
 $u(x, t)$

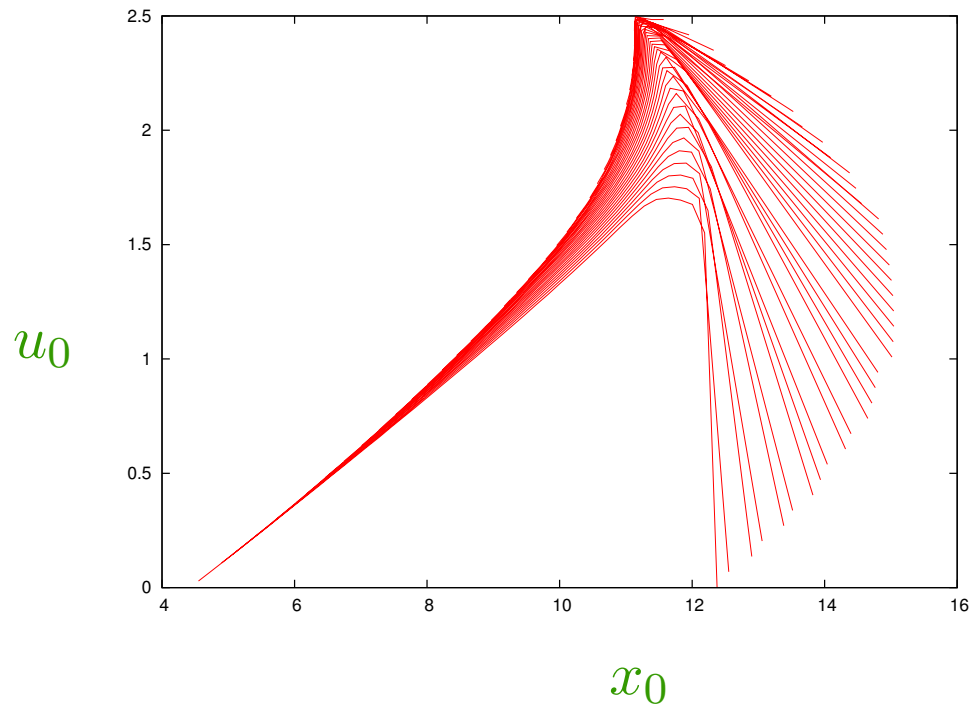


# Deceleration:

Small slope, so initial conditions decelerate with  $\mu g$ :

$$u = u_0(x_0) - \mu g(t - t_0)$$

$$x = x_0 + u_0(x_0)(t - t_0) - \frac{1}{2}\mu g(t - t_0)^2$$



# Extension of runout during deceleration

Decelerate from  $u = u_3 = 2\sqrt{gR_0}a^{1/6}$

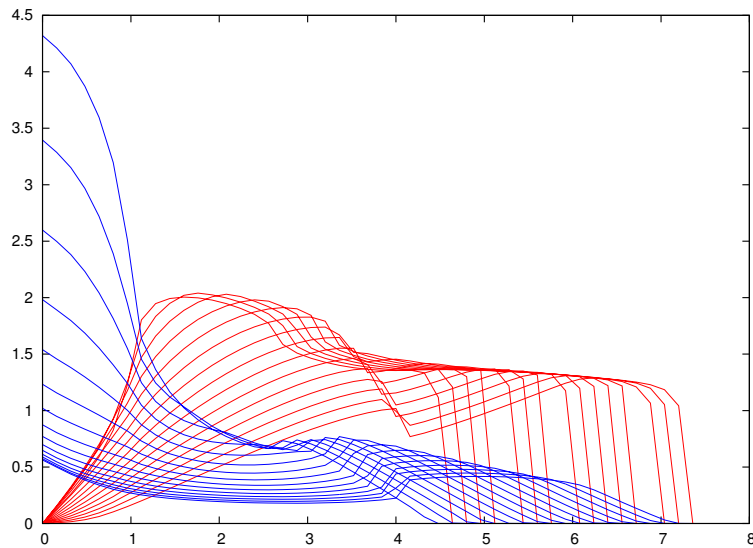
at  $\mu g$

in distance  $3.5a^{1/3}$

# Axisymmetric similar

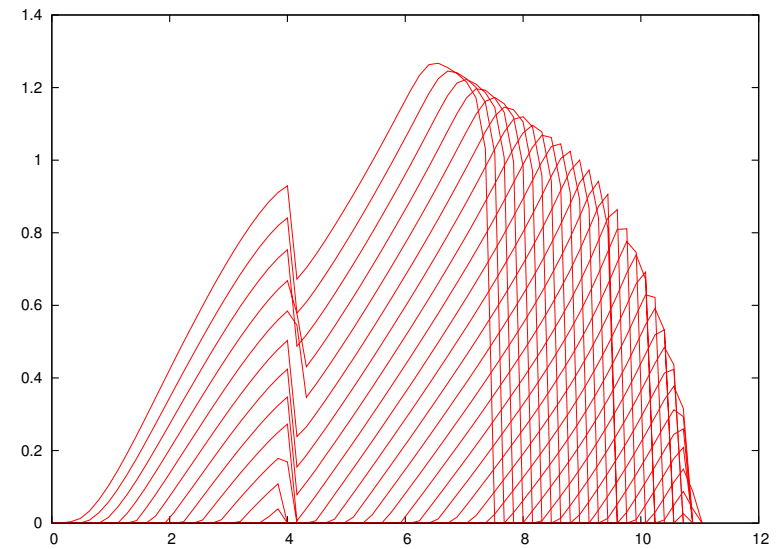
## Propagating wave

$$4.3 < t < 6.3 \quad a = 9.1$$



## Deceleration

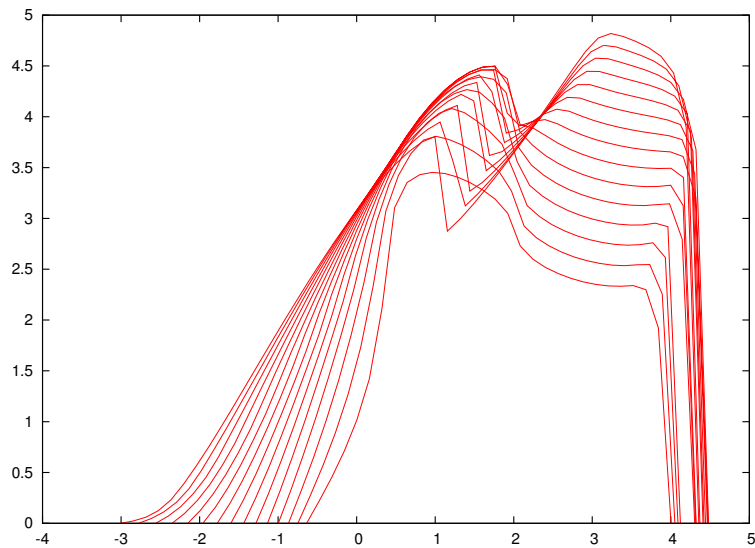
$$6.5 < t < 11 \quad a = 9.1$$



# Axisymmetric similar

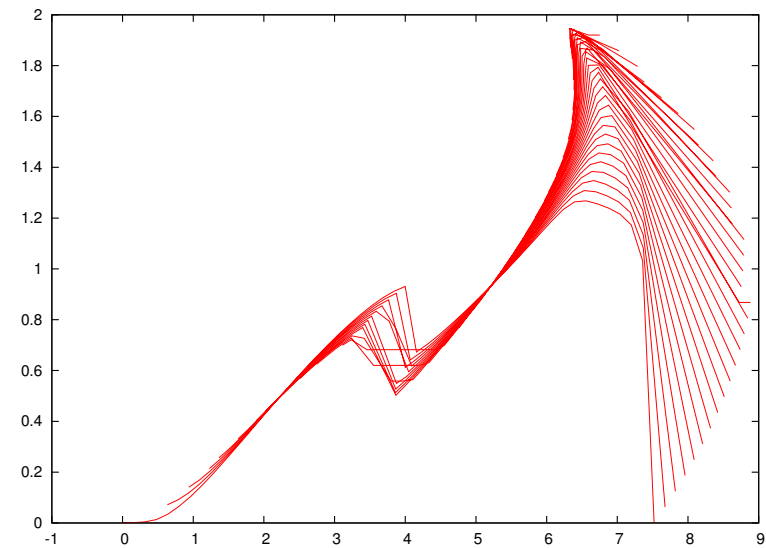
Propagating wave

$$u\alpha(t)$$



Deceleration

$$u_0(x_0)$$



# A little explanation?

## Three phases

- Leaving the base

Runout	$1.1R_0a^{2/3}$ (2D)	$1.5R_0a^{1/2}$ (Axi)
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- Propagating wave

	$+2.2R_0a^{1/2}$	$+1.6R_0a^{1/4}$
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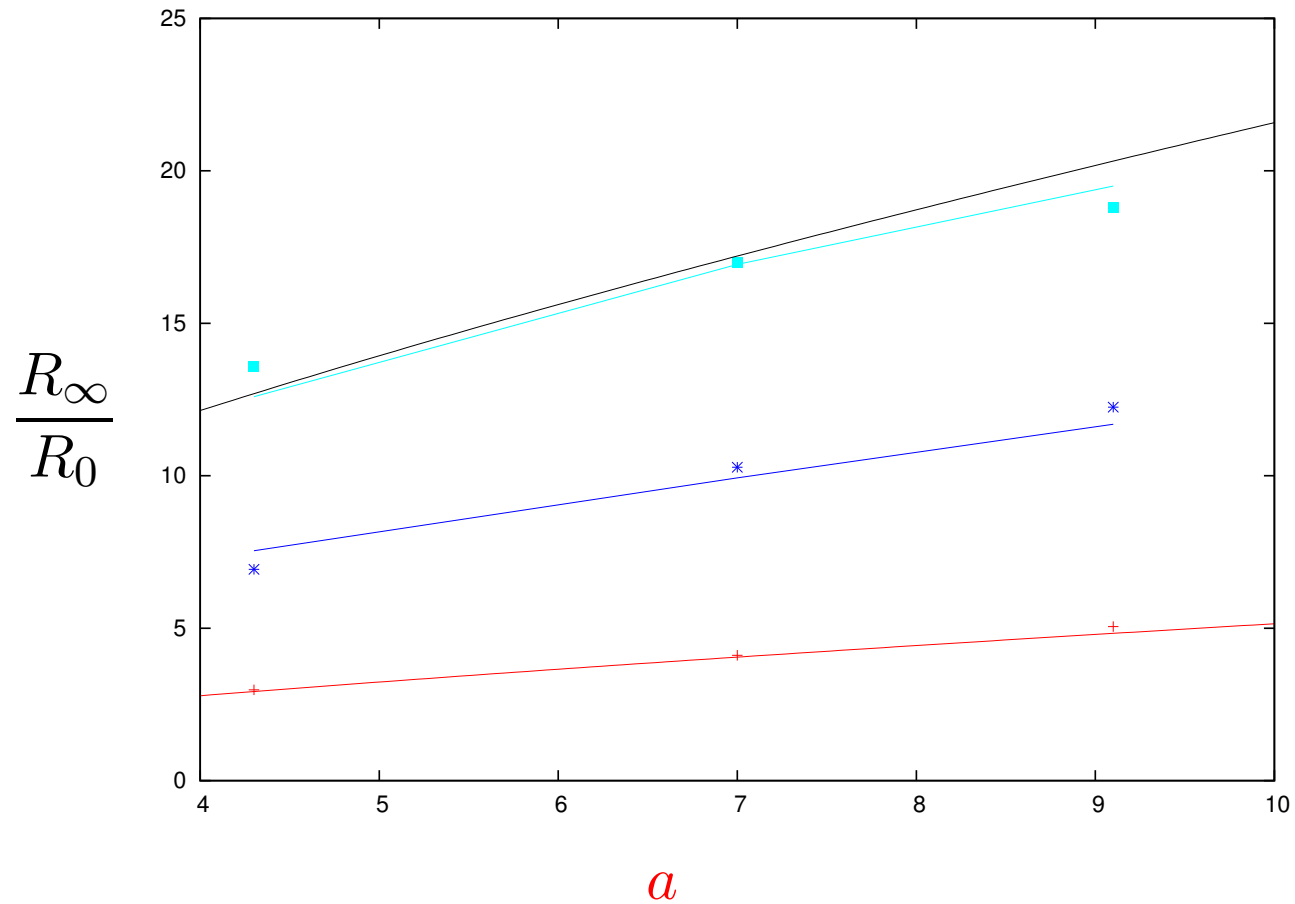
- Deceleration

	$+3.5R_0a^{1/3}$	$+3.7R_0$
--	------------------	-----------



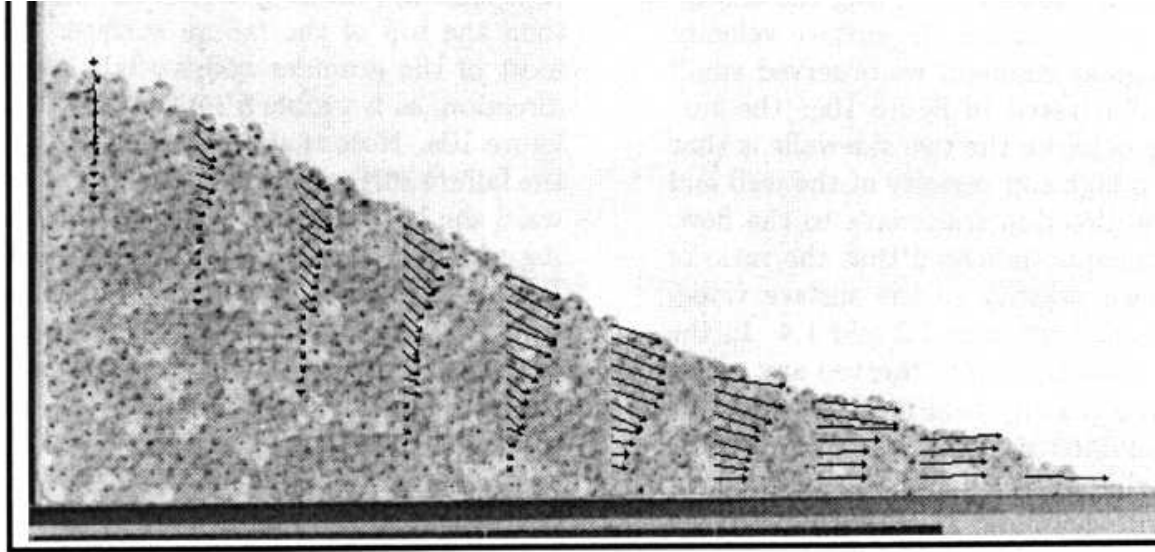
# A little explanation?

Three phases, 2D





# But, the velocity profile



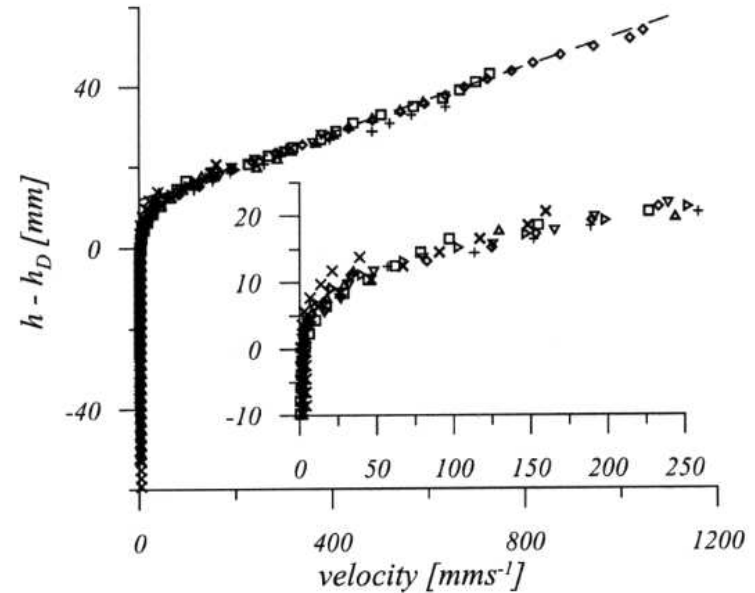
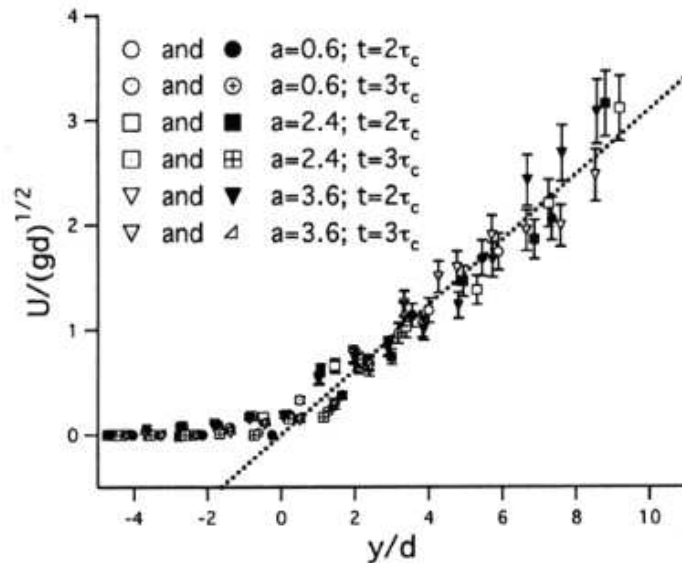
Lajeunesse, Monnier & Homsy 2005 PoF

Linear over stationary

Approx plug near front

# But, the velocity profile

Linear profile on top of stationary layer

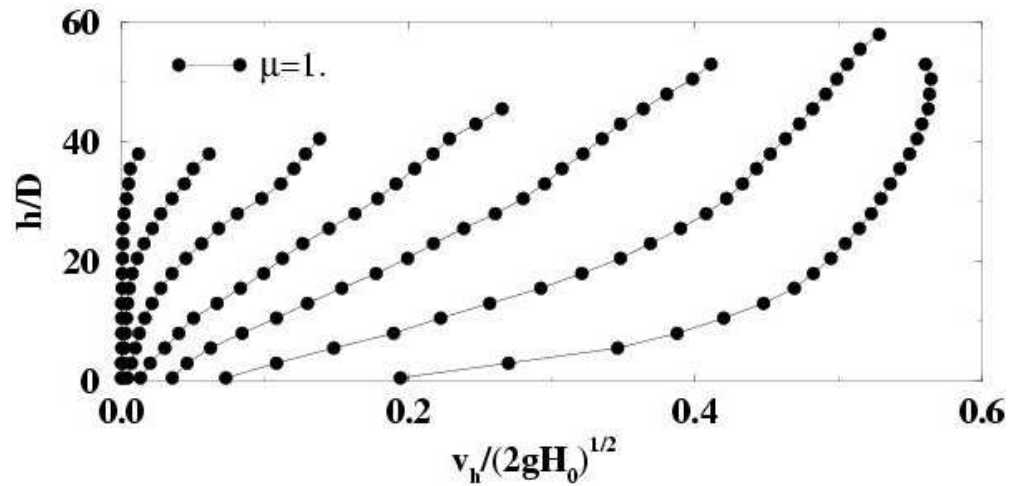
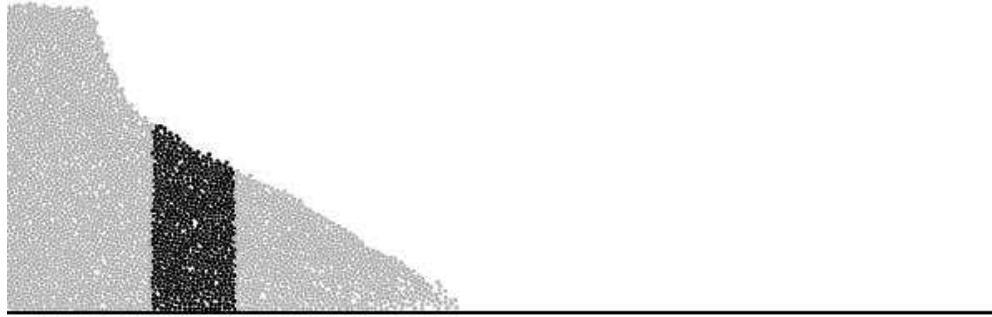


Lajeunesse, Monnier & Homsy 2005 PoF Lube, Huppert, Freundt & Sparks 2006 PoF

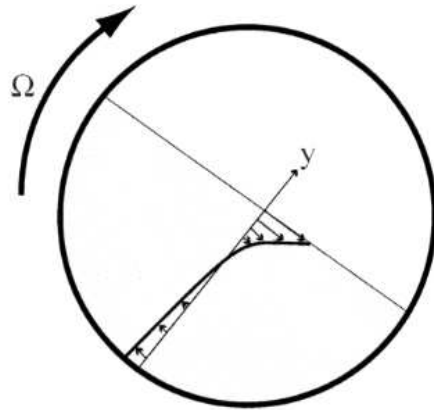
$$\gamma = 0.3 \sqrt{g/d}, \quad \text{indpt } a$$

$$\gamma = 7 \sqrt{g/H_0}, \quad \text{indpt } a$$

# But, the velocity profile

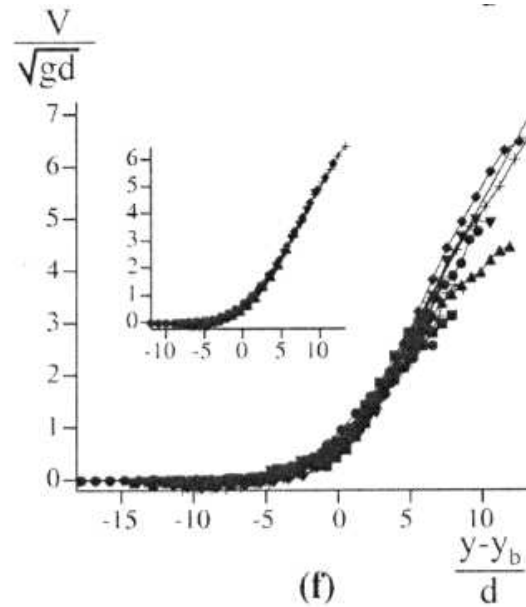


# Linear profile in another geometry



GDR MiDi 2004 EPJ-E

$$\gamma = 0.5\sqrt{g/d}$$



# Evolving profile?

If flat and  $u(y, t)$

$$\text{Hydrostatic : } \sigma_{zz} = -\rho g(h - z)$$

$$\text{Friction : } \sigma_{xz} = -\mu\sigma_{zz}$$

$$\text{So } \rho \frac{\partial u}{\partial t} = \frac{\partial \sigma_{xz}}{\partial z} = -\mu\rho g$$

Solution

$$u(y, t) = \max(u(y, 0) - \mu g t, 0)$$

Linear profile remains linear at same shear-rate,  
depth of stationary layer grows at  $\dot{y} = \mu g / \gamma$

# But, the velocity profile

- Linear profile over stationary layer
  - just final stopping?
  - low flux?
- Plug profile near front
  - high flux?
  - main runout?
- Change shallow-water  $\beta = \frac{4}{3}$ 
  - shorter runout?
  - change  $K$  also?