#### Small particles in a viscous fluid

John Hinch

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## Small particles in a viscous fluid

Course in three parts

- 1. A quick course in micro-hydrodynamics
- 2. Sedimentation of particles
- 3. Rheology of suspensions

Good textbook for parts 1 & 2: A Physical Introduction to Suspension Dynamics by Elisabeth Guazzelli, Jeffrey F. Morris and Sylvie Pic (Cambridge Texts in Applied Mathematics 2012).

# A quick course in micro-hydrodynamics

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[Simple properties](#page-23-0)

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# A quick course in micro-hydrodynamics

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So Cauchy momentum equation

$$
\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = \nabla \cdot \boldsymbol{\sigma} + \mathbf{F}
$$

Newtonian viscous fluids

<span id="page-9-0"></span>
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e_{ij} = \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right)
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Note this is the most general relationship between  $\sigma$  and  $\nabla$ **u** which is linear, instantaneous and isotropic.

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Hence the Navier-Stokes equation (momentum for a Newtonian viscous fluid) assuming  $\mu$  constant.

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Boundary conditions

$$
\mathbf{u}(\mathbf{x}) \quad \text{given, or} \quad \boldsymbol{\sigma} \cdot \mathbf{n}(\mathbf{x}) \quad \text{given}
$$

For a flow  $U$  over distances  $L$ , the Reynolds number is

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- e.g.  $1 \mu m$  water droplet falls under gravity in air at  $0.1 \text{ mm/s}$ , so  $Re = 10^{-5}$ .

If  $Re \ll 1$ , then Stokes flow (also called "creeping flow")

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Note: Stokes theory for  $Re \ll 1$  usually works for  $Re < 2$ .

## A quick course in micro-hydrodynamics

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1. Linear and Instantaneous

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E.g. Rigid particle translation at  $U(t)$  in unbounded fluid Flow  $\mathbf{u}(\mathbf{x},t)$  linear & instantaneous in  $\mathbf{U}(t)$ , also  $\sigma(\mathbf{x},t)$ , hence drag force

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Apply force  $F(t)$  in  $0 \le t \le t_1$ . Now reverse force and its history, i.e.  $F(t) = -F(2t_1 - t)$  in  $t_1 \leq t \leq 2t_1$ 

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Hence cannot swim at  $Re \ll 1$  by reversible flapping.

3. Reversible in space:

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E.g. 4. Two rigid spheres in a shear flow (possibly unequal, possibly next to a rigid wall) resume their original undisturbed streamlines after a collision.
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<span id="page-37-0"></span>Uniform flow U past a rigid sphere of radius a.

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\mathbf{u} = \mathbf{U} \left( 1 - \frac{3a}{4r} - \frac{a^3}{4r^3} \right) + \mathbf{x} (\mathbf{U} \cdot \mathbf{x}) \left( -\frac{3a}{4r^3} + \frac{3a^3}{4r^5} \right),
$$

$$
p = -\frac{3a\mu \mathbf{U} \cdot \mathbf{x}}{2r^3} \quad \text{and} \quad \sigma \cdot \mathbf{n}|_{r=a} = \frac{3\mu}{2a} \mathbf{U}.
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$$

Hence the Stokes drag on the sphere is

$$
\int_{r=a} \sigma \cdot \mathbf{n} \, dS = 4\pi a^2 \, \frac{3\mu}{2a} \mathbf{U} = 6\pi \mu a \mathbf{U}.
$$

## 2. Solution method 1

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The velocity and pressure fields must therefore take the forms

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\begin{array}{rcl}\n\mathbf{u}(\mathbf{x}) & = & \mathbf{U}f(r) + \mathbf{x}(\mathbf{U}\cdot\mathbf{x})g(r), \\
p(\mathbf{x}) & = & \mu(\mathbf{U}\cdot\mathbf{x})h(r),\n\end{array}
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where  $r = |\mathbf{x}|$ , and f, g and h are functions of scalar r to be determined.

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Now

$$
\frac{\partial u_i}{\partial x_j} = U_i x_j f'/r + \delta_{ij} U_n x_n g + x_i U_j g + x_i x_j U_n x_n g'/r.
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Substituting, one finds  $\alpha = 0, -3$  and  $-5$ , with associated  $f=-(\alpha+4)r^{\alpha+2}/(\alpha+2)$  and  $h=-(\alpha+5)(\alpha+2)r^{\alpha}$ .

solution method 1

Hence the general solution of the assumed form linear in  $\boldsymbol{u}$  is

$$
\mathbf{u}(\mathbf{x}) = \mathbf{U} \left( -2Ar^2 + B + Cr^{-1} - \frac{1}{3}Dr^{-3} \right) + \mathbf{x}(\mathbf{U} \cdot \mathbf{x}) \left( A + Cr^{-3} + Dr^{-5} \right),
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We shall need the stress exerted across a spherical surface with unit normal  $\mathbf{n} = \mathbf{x}/r$ 

$$
\boldsymbol{\sigma}\!\cdot\! \mathbf{n} = \mathbf{U}\left(-3A r + 2D r^{-4}\right) + \mathbf{x}(\mathbf{U}\!\cdot\! \mathbf{x})\left(9A r^{-1} - 6C r^{-4} - 6D r^{-6}\right)
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We shall need the stress exerted across a spherical surface with unit normal  $\mathbf{n} = \mathbf{x}/r$ 

$$
\boldsymbol{\sigma} \cdot \mathbf{n} = \mathbf{U} \left( -3Ar + 2Dr^{-4} \right) + \mathbf{x} (\mathbf{U} \cdot \mathbf{x}) \left( 9Ar^{-1} - 6Cr^{-4} - 6Dr^{-6} \right)
$$

Applying the boundary conditions on the rigid sphere and for the far field, we find the coefficients

$$
A = 0
$$
,  $B = 1$ ,  $C = -\frac{3}{4}a$  and  $D = \frac{3}{4}a^3$ 

#### For solution given earlier

Use a Stokes streamfunction for the axisymmetric flow

<span id="page-54-0"></span>
$$
u_r = \frac{1}{r^2 \sin \theta} \frac{\partial \Psi}{\partial \theta} \quad \text{and} \quad u_{\theta} = -\frac{1}{r \sin \theta} \frac{\partial \Psi}{\partial r}.
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The vorticity equation (curl of the momentum equation, to eliminate the pressure) is then at low Reynolds numbers

$$
\mathcal{D}^2 \mathcal{D}^2 \Psi = 0 \quad \text{where} \quad \mathcal{D}^2 = \frac{\partial^2}{\partial r^2} + \frac{\sin \theta}{r^2} \frac{\partial}{\partial \theta} \left( \frac{1}{\sin \theta} \frac{\partial}{\partial \theta} \right).
$$

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$$

The uniform flow at infinity has  $\Psi = \frac{1}{2} U r^2 \sin^2 \theta$ , so one tries  $\Psi = F(r) \sin^2 \theta$ , and finds  $F = Ar^4 + Br^2 + Cr + D/r$ .

One can show (Papkovich-Neuber) that the general solution of the Stokes equation can be expressed in terms of a vector harmonic function  $\phi(\mathbf{x})$  (i.e.  $\nabla^2 \phi = 0$ )

<span id="page-57-0"></span>
$$
\mathbf{u} = 2\phi - \nabla(\mathbf{x} \cdot \phi) \quad p = -2\mu \nabla \cdot \phi.
$$

$$
\sigma_{ij} = 2\mu \left( \delta_{ij} \frac{\partial \phi_n}{\partial x_n} - x_k \frac{\partial^2 \phi_k}{\partial x_i \partial x_j} \right).
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$$

Linearity and spherical symmetry then give

$$
\phi = A \mathbf{U} \frac{1}{r} + B \mathbf{U} \cdot \nabla \nabla \frac{1}{r},
$$

with coefficients A and B to be determined by applying the boundary conditions.

The pressure and vorticity are harmonic functions.

Using linearity and spherical symmetry, they must take the form

<span id="page-59-0"></span>
$$
p = \mu A \mathbf{U} \cdot \mathbf{x} / r^3
$$
 and  $\nabla \wedge \mathbf{u} = B \mathbf{U} \wedge \mathbf{x} / r^3$ .

The final step to **u** is tedious.

Force balance, with densities  $\rho_s$  of sphere and  $\rho_f$  of fluid

<span id="page-60-0"></span>
$$
0 = \rho_s \frac{4\pi}{3} a^3 g - \rho_f \frac{4\pi}{3} a^3 g - 6\pi \mu a
$$
  
no inertia weight buoyancy Stokes drag

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So Stokes settling velocity

$$
U=\frac{2\Delta\rho a^2g}{9\mu}
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E.g.  $1\,\mu\mathrm{m}$  sphere,  $\Delta\rho=10^3\,\mathrm{kg\,m^{-3}}$ , water  $\mu=10^{-3}\,\mathrm{Pa\,s}$ gives  $U = 2 \mu m/s$ , i.e. falls through diameter in a second.

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Drag on a fluid sphere (Student exercise!)

$$
\mathbf{F} = -2\pi \frac{2\mu_f + 3\mu_s}{\mu_f + \mu_s} \mu_f aU
$$

Sphere rotating at angular velocity  $\Omega$ . Flow

<span id="page-65-0"></span>
$$
\mathbf{u}(\mathbf{x}) = \mathbf{\Omega} \wedge \mathbf{x} \frac{a^3}{r^3}
$$

(A potential flow, so satisfies Stokes equations.)

Sphere rotating at angular velocity  $\Omega$ . Flow

$$
\mathbf{u}(\mathbf{x}) = \mathbf{\Omega} \wedge \mathbf{x} \frac{a^3}{r^3}
$$

(A potential flow, so satisfies Stokes equations.) Hence couple on sphere – student exercise!

$$
\mathbf{G}=8\pi\mu a^3\mathbf{\Omega}
$$

<span id="page-67-0"></span>For principle semi-diameters  $a_1$ ,  $a_2$ ,  $a_3$  Oberbeck (1876) found

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$$
\text{Force} \quad F_1 = -\frac{16\pi\mu U_1}{L + a_1^2 K_2} \quad \text{and Couple} \quad G_1 = -\frac{16\pi\mu (a_2^2 + a_3^2)}{3(a_2^2 K_2 + a_3^2 K_3)}
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where

$$
L = \int_0^\infty \frac{d\lambda}{\Delta(\lambda)} \quad \text{and} \quad K_i = \int_0^\infty \frac{d\lambda}{(a_i^2 + \lambda)\Delta(\lambda)}
$$
  
with  $\Delta^2 = (a_1^2 + \lambda)(a_3^2 + \lambda)(a_3^2 + \lambda)$ .

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with  $\Delta^2 = (a_1^2 + \lambda)(a_3^2 + \lambda)(a_3^2 + \lambda)$ .  
For a disk  $a_1 \ll a_2 = a_3$   
 $F_1 \sim 16\pi \mu a_2 U_1$ ,  $F_2 \sim \frac{32}{3} \mu a_2 U_2$ ,  $G_i \sim \frac{8}{3} \mu a_2 \Omega_i$ 

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For a rod  $a_1 \gg a_2 = a_3$ , where  $\ln = \ln \frac{2a_1}{a_2}$   
 $F_1 \sim \frac{4\pi \mu a_1 U_1}{\ln - \frac{1}{2}}$ ,  $F_2 \sim \frac{8\pi \mu a_1 U_2}{\ln + \frac{1}{2}}$ ,  $G_1 \sim \frac{16}{3} \pi \mu a_1 a_2 \Omega_1$ ,  $G_2 \sim \frac{\frac{8}{3} \pi \mu a_1^3 \Omega}{\ln - \frac{1}{2}}$
#### Stokes flow past an ellipsoid

For principle semi-diameters  $a_1, a_2, a_3$  Oberbeck (1876) found

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$$
F_1 = -\frac{16\pi\mu U_1}{L + a_1^2 K_2}
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 and Couple  $G_1 = -\frac{16\pi\mu(a_2^2 + a_3^2)}{3(a_2^2 K_2 + a_3^2 K_3)}$ 

where

 $L = \int_{-\infty}^{\infty}$ 0  $d\lambda$  $\frac{d\lambda}{\Delta(\lambda)}$  and  $K_i =$  $\int^{\infty}$ 0  $d\lambda$  $(a_i^2 + \lambda)\Delta(\lambda)$ with  $\Delta^2 = (a_1^2 + \lambda)(a_3^2 + \lambda)(a_3^2 + \lambda)$ . For a disk  $a_1 \ll a_2 = a_3$  $F_1 \sim 16\pi\mu$ a<sub>2</sub> $U_1$ ,  $F_2 \sim \frac{32}{3}$  $\frac{32}{3}\mu$ a<sub>2</sub>U<sub>2</sub>, G<sub>i</sub> ~  $\frac{8}{3}$  $\frac{8}{3}\mu$ a2Ω<sub>i</sub> For a rod  $a_1 \gg a_2 = a_3$ , where  $\ln = \ln \frac{2a_1}{a_2}$  $\mathcal{F}_1 \sim \frac{4\pi\mu a_1 U_1}{1}$  $\ln -\frac{1}{2}$ 2  $F_2 \sim \frac{8\pi\mu a_1 U_2}{1}$  $\ln +\frac{1}{2}$  $, \quad G_1 \sim \frac{16}{3}$  $\frac{16}{3}\pi\mu$ a<sub>1</sub>a<sub>2</sub> $\Omega_1$ ,  $G_2 \sim$ 8  $\frac{8}{3}π\mu a_1^3\Omega_2$  $\ln -\frac{1}{2}$ 2

Important conclusion Drag  $\approx 6\pi\mu$  with largest diameter.

## A quick course in micro-hydrodynamics

[Stokes equations](#page-3-0)

[Simple properties](#page-23-0)

[Flow past a sphere](#page-36-0)

#### [More simple properties](#page-73-0)

[A useful result](#page-74-0) [Minimum dissipation](#page-78-0) **[Uniqueness](#page-86-0)** [Geometric bounding](#page-93-0) [Reciprocal theorem](#page-103-0) [Symmetry of resistance matrix](#page-108-0) [Faxen's formula](#page-116-0)

#### <span id="page-73-0"></span>[Greens function](#page-132-0)

1. A useful result

Let  ${\bf u}^S({\bf x})$  be a Stokes flow with  ${\bf F}=0$  in  $V$ , and let  ${\bf u}({\bf x})$  be any other incompressible flow, then

<span id="page-74-0"></span>
$$
\int_V 2\mu e_{ij}^Se_{ij} dV = \int_S \sigma_{ij}^Sn_j u_i dA.
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Because

$$
2\mu e_{ij}^{S} = \sigma_{ij}^{S} + p^{S} \delta_{ij} \text{ and } p^{S} \delta_{ij} e_{ij} = p^{S} \nabla \cdot \mathbf{u} = 0 \qquad (1)
$$
  
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2\mu e_{ij}^{S} e_{ij} = \sigma_{ij}^{S} e_{ij}.
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$$

$$
\text{so} \quad 2\mu \epsilon_{ij}^S \epsilon_{ij} = \sigma_{ij}^S \epsilon_{ij}.\tag{2}
$$

And

$$
\sigma_{ij}^S = \sigma_{ji}^S \quad \text{so} \tag{3}
$$

$$
\sigma_{ij}^{S} e_{ij} = \sigma_{ij}^{S} \frac{\partial u_{i}}{\partial x_{j}} = \frac{\partial}{\partial x_{j}} \left( \sigma^{S} i j u_{i} \right) - \frac{\partial \sigma_{ij}^{S}}{\partial x_{j}} u_{i}
$$
(4)

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$$
(4)

Hence result by divergence theorem.

2. Minimum dissipation

<span id="page-78-0"></span>Let  $\mathbf{u}(\mathbf{x})$  and  $\mathbf{u}^{S}(\mathbf{x})$  be two incompressible flows in  $V$ , both satisfying the same boundary condition  $\mathbf{u}=\mathbf{u}^\mathcal{S}=\mathbf{U}(\mathbf{x})$  give on  $\mathcal{S}.$ 

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$$
\int_{V} 2\mu e_{ij} e_{ij} dV = \int_{V} 2\mu e_{ij}^{S} e_{ij}^{S} dV
$$

$$
+ \int_{V} 2\mu (e_{ij} - e_{ij}^{S})(e_{ij} - e_{ij}^{S}) dV + \int_{V} 4\mu e_{ij}^{S}(e_{ij} - e_{ij}^{S}) dV.
$$
  
 
$$
\leftarrow \text{positive} \rightarrow
$$

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$$
\int_V 2\mu e_{ij}e_{ij} dV = \int_V 2\mu e_{ij}^S e_{ij}^S dV
$$

$$
+ \int_V 2\mu (e_{ij} - e_{ij}^S)(e_{ij} - e_{ij}^S) dV + \int_V 4\mu e_{ij}^S (e_{ij} - e_{ij}^S) dV.
$$

The last integral is of the form of the useful result

$$
\int_V 4\mu e_{ij}^S(e_{ij}-e_{ij}^S) dV = \int_S 2\sigma_{ij}^S n_j(u_i-u_i^S) dA = 0 \text{ by bc}
$$

2. Minimum dissipation

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$$
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Hence e.g. drag larger at non-zero Reynolds number.

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Hence e.g. drag larger at non-zero Reynolds number.

Warning: Same geometry. Cannot select geometry by minimum dissipation.

3. Uniqueness

If  $\mathsf{u}^1(\mathsf{x})$  and  $\mathsf{u}^2(\mathsf{x})$  are two Stokes flows in  $V$  satisfying the same boundary conditions, then minimum dissipation gives

<span id="page-86-0"></span>
$$
\int_V 2\mu (e_{ij}^1-e_{ij}^2)(e_{ij}^1-e_{ij}^2)\,dV=0
$$

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Hence Stokes flows are unique.

4. Geometric bounding

<span id="page-93-0"></span>Rigid cube, sides of length  $2L$ , moving at U, drag F.

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$$
\int_V 2\mu e_{ij}^S e_{ij}^S dV = \text{rate of working by surface forces} = -\mathbf{U} \cdot \mathbf{F}.
$$

4. Geometric bounding

Rigid cube, sides of length  $2L$ , moving at U, drag F. Let  $\mathbf{u}^{S}(\mathbf{x})$  be Stokes flow outside cube, V. Then dissipation

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Cube just contained by sphere radius  $a =$ √ 3L, also moving at  $\bm{\mathsf{U}}$ .

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Define second flow

$$
\mathbf{u}(\mathbf{x}) = \begin{cases} \text{the Stokes flow for sphere} & \text{outside sphere,} \\ \mathbf{U} & \text{in gap.} \end{cases}
$$

4. Geometric bounding

For this second flow

$$
\int_{V} 2\mu e_{ij} e_{ij} dV = \int_{r>a} 2\mu e_{ij} e_{ij} dV \text{ because } e = 0 \text{ in gap,}
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 $6\pi\mu L$ U·U  $\leq -F \cdot U$ 

Student exercises: bound for tetrahedron (not so tight).

5. Reciprocal theorem

<span id="page-103-0"></span>For the same volume V, let  $u_1$  be the Stokes flow with volume forces  $f_1$  satisfying boundary conditions  $u_1 = U_1$ .

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Then by the useful result

$$
\int_{V} \mathbf{u}_{1} \cdot \mathbf{f}_{2} dV + \int_{S} \mathbf{U}_{1} \cdot \boldsymbol{\sigma}_{2} \cdot \mathbf{n} dA = \int_{V} 2\mu \mathbf{e}_{1} : \mathbf{e}_{2} dV
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Greens theorem in any other subject
6. Reciprocal theorem – application to resistance matrix

General rigid body motion in fluid at rest a infinity, translating at  $U(t)$  and rotating (about a selected point)  $\Omega(t)$ .

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General rigid body motion in fluid at rest a infinity, **translating at U(t) and rotating** (about a selected point)  $\Omega(t)$ . By linearity and instantaneity, the force  $F(t)$  and couple  $G(t)$ (about the same selected point)

$$
\begin{pmatrix} \boldsymbol{F} \\ \boldsymbol{G} \end{pmatrix} = \begin{pmatrix} \boldsymbol{A} \ \boldsymbol{B} \\ \boldsymbol{C} \ \boldsymbol{D} \end{pmatrix} \begin{pmatrix} \boldsymbol{U} \\ \boldsymbol{\Omega} \end{pmatrix}
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The Reciprocal theorem gives for the two rigid body motions

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\textbf{U}_1\!\cdot\!\textbf{F}_2+\boldsymbol{\Omega}_1\cdot\textbf{G}_2=\textbf{U}_2\!\cdot\!\textbf{F}_1+\boldsymbol{\Omega}_2\cdot\textbf{G}_1
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True all  $\mathbf{U}_1$  etc, so

$$
A = A^T, \quad B = C^T \quad \text{and} \quad D = D^T.
$$

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Need "corkscrew" feature for  $B \neq 0$ .

7. Reciprocal theorem – application to Faxen's formula

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Applying Reciprocal theorem

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\int u_1 \cdot \mathbf{f}_2 \ dV + \int u_1 \cdot \mathbf{\sigma}_2 \cdot \mathbf{n} \ dA = \int u_2 \cdot \mathbf{f}_1 \ dV + \int \mathbf{u}_2 \cdot \mathbf{\sigma}_1 \cdot \mathbf{n} \ dA.
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Now look at RHS and then LHS, using  $\mathbf{u}_1 = \mathbf{u}^+ - \mathbf{u}^{\infty}$ .

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\mathrm{RHS} = \boldsymbol{\mathsf{U}}_2 \cdot \left( \int \boldsymbol{\sigma}^+ \cdot \boldsymbol{\mathsf{n}} \, dA - \int \boldsymbol{\sigma}^\infty \cdot \boldsymbol{\mathsf{n}} \, dA = 0 - 0 \right) = 0,
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as both integrals are force on sphere.

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$$
\mathrm{LHS} = -\frac{3\mu}{a} \boldsymbol{\mathsf{U}}_2 \cdot \left( \int \underset{= \mathsf{V}} {\boldsymbol{\mathsf{u}}}^+ \, dA - \int \boldsymbol{\mathsf{u}}^\infty \, dA \right) = \mathrm{RHS} = 0
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$$

For all  $\mathbf{U}_2$ , so velocity of sphere inserted into  $\mathbf{u}^{\infty}(\mathbf{x})$  is

$$
\mathbf{V} = \frac{1}{4\pi a^2} \int_{r=a} \mathbf{u}^{\infty}(\mathbf{x}) dA
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Finally use a Taylor series

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\mathbf{u}^{\infty}(\mathbf{x}) = \mathbf{u}^{\infty}(0) + \mathbf{x} \cdot \nabla \mathbf{u}^{\infty} \vert_0 + \frac{1}{2} \mathbf{x} \mathbf{x} : \nabla \nabla \mathbf{u}^{\infty} \vert_0 + \cdots
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with higher even terms vanishing by  $\nabla^{2n}(\mathsf{Stokes}\;{\text{equations}})=0.$ 

# A quick course in micro-hydrodynamics

[Stokes equations](#page-3-0)

[Simple properties](#page-23-0)

[Flow past a sphere](#page-36-0)

[More simple properties](#page-73-0)

[Greens function](#page-132-0) **[Stokeslet](#page-133-0)** [Integral representation](#page-141-0) [Slender-body theory](#page-156-0)

<span id="page-132-0"></span>[Effect of small inertia](#page-161-0)

or 'Stokeslet'

For a point momentum source

<span id="page-133-0"></span>
$$
\nabla \cdot \mathbf{u} = 0
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0 = -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F} \delta(\mathbf{x})
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Solution – more important than derivation

$$
\mathbf{u}(\mathbf{x}) = \mathbf{F} \cdot \mathbf{G}(\mathbf{x}) = \frac{1}{8\pi\mu} \left( \mathbf{F} \frac{1}{r} + (\mathbf{F} \cdot \mathbf{x}) \mathbf{x} \frac{1}{r^3} \right)
$$

$$
\sigma(\mathbf{x}) = \mathbf{F} \cdot \mathbf{K}(\mathbf{x}) = -\frac{3}{4\pi} \mathbf{F} \cdot \mathbf{x} \mathbf{x} \mathbf{x} \frac{1}{r^5}
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G is called the 'Oseen tensor'.

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Already seen this in flow past a sphere:

Far field for a sphere

Far from the sphere  $r \gg a$ , the flow is

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$$
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#### Greens function for Stokes equations Far field for a sphere

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$$

But the drag is  $\mathbf{F} = -6\pi\mu a \mathbf{U}$ , i.e.

$$
\mathbf{u} - \mathbf{U} \sim \frac{1}{8\pi\mu} \left( \mathbf{F} \frac{1}{r} + (\mathbf{F} \cdot \mathbf{x}) \mathbf{x} \frac{1}{r^3} \right)
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$$

Hence far-field due to force is universal, independent of particle shape.

Integral representation

To solve

<span id="page-141-0"></span>
$$
\nabla \cdot \mathbf{u} = 0
$$

$$
0 = -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{f}(\mathbf{x})
$$

with boundary conditions on  $\mathbf{u}(\mathbf{x})$  or  $\sigma(\mathbf{x})\cdot\mathbf{n}$ .

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Use the Reciprocal theorem (Greens theorem) with  $\mathbf{u}_1$  for the unknown flow and  $\mathbf{u}_2$  for the Greens function for point source at  $\mathbf{x}'$ 

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$$
\mathbf{u}(\mathbf{x}') = \int_{V} \mathbf{G}(\mathbf{x} - \mathbf{x}') \cdot \mathbf{f} dV
$$
  
forces in *V*  
+ 
$$
\int_{S} \left( \mathbf{G}(\mathbf{x} - \mathbf{x}') \cdot \boldsymbol{\sigma}(\mathbf{x}) \cdot \mathbf{n} - (\mathbf{K}(\mathbf{x} - \mathbf{x}') \cdot \mathbf{n}) \cdot \mathbf{u} \right) dA
$$
  
forces on *S* dipoles on *S*
Integral representation – Boundary integral Method

Letting  $x'$  in  $V$  tend onto the surface  $S$  yields an integral equation for the unknown **u** (or  $\sigma \cdot n$ ) on S in terms of the known  $\sigma \cdot n$  (or **u**) on S.

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Delicate limit  $\mathsf{x}'\to \mathsf{S}\colon \int \mathsf{K}\!\cdot\! \mathsf{n} \to +\frac{1}{2}$  $\frac{1}{2}$ **u** for **x**' in *V*,

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\frac{1}{2}(1+\lambda)\mathbf{u}(\mathbf{x}') = \mathbf{u}^{\infty}(\mathbf{x}')
$$

$$
-\int_{S} \mathbf{G}(\mathbf{x}-\mathbf{x}') \cdot \gamma \kappa \mathbf{n} dA - (1-\lambda) \int_{S} \mathbf{K}(\mathbf{x}-\mathbf{x}') \cdot \mathbf{n} \cdot \mathbf{u} dA
$$

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or asymptotically for

$$
\mathbf{f}(s_0) \sim \frac{2\pi\mu}{\ln\frac{L}{R}}\left(2\mathbf{I} - \mathbf{X}'\mathbf{X}'\right) \cdot \left(\mathbf{U}(s_0) - \mathbf{u}^{\infty}(\mathbf{X}(s_0))\right)
$$

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which does not decay.

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Solve by Fourier transforms or representation

$$
\mathbf{u}' = \nabla \phi + \nu \nabla \chi - \mathbf{U} \chi \quad \text{and} \quad p' = -\rho \mathbf{U} \cdot \nabla \phi.
$$

Oseen equation solved

Find

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\phi = -\frac{3a\nu}{2r} \text{(point volume source)} \quad \text{and} \quad \chi = \frac{3a}{2r} e^{\left(\frac{0x}{2\nu} - \frac{0r}{2\nu}\right)}
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Hence drag increases by  $1+\frac{3}{8}Re$ .

Look far from sphere  $r \gg \nu/U$  near downstream axis

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Missing mass flux in wake goes to point source  $\phi$ -flow.

# A quick course in micro-hydrodynamics

[Stokes equations](#page-3-0)

[Simple properties](#page-23-0)

[Flow past a sphere](#page-36-0)

[More simple properties](#page-73-0)

[Greens function](#page-132-0)

[Effect of small inertia](#page-161-0)