

# Instabilities of a thin coating on a vertical fibre; Newtonian, shear-thinning, and elastic liquids

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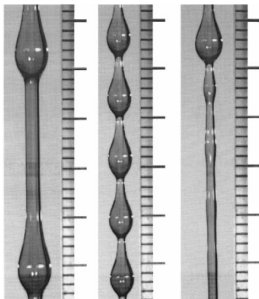
CMS-DAMTP, University of Cambridge

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and Claire McIlroy for elastic liquids

# Motivation

Manufacture of polymeric and optical fibres.



Newtonian

Kliakhandler, Davis & Bankoff JFM 2001



Shear-thinning

Duprat, Ruyer-Quil & Giorgiutti-Dauphiné

Phys. Fluids 2009

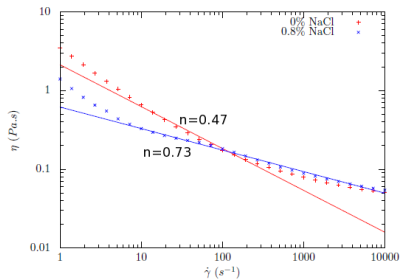
The coating fluid is often non-Newtonian

# Governing equations

## Constitutive equation

$$\text{Power-law viscosity: } \mu = \beta \left| \frac{\partial u}{\partial y} \right|^{n-1}$$

Xanthan solutions



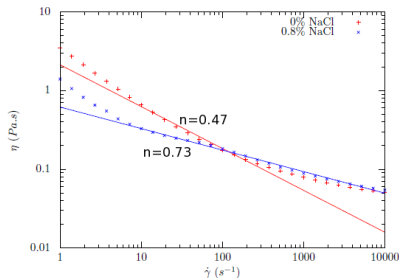
Boulogne et al, Private Communication

# Governing equations

## Constitutive equation

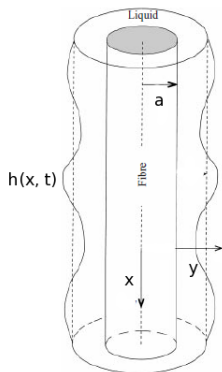
$$\text{Power-law viscosity: } \mu = \beta \left| \frac{\partial u}{\partial y} \right|^{n-1}$$

Xanthan solutions



Boulogne et al, Private Communication

Geometry  
Axisymmetric



# Governing equations

## Lubrication framework

Capillary pressure:  $p = -\gamma \left( \frac{h}{a^2} + h_{xx} \right)$

Momentum:  $0 = -\frac{dp}{dx} + \rho g + \frac{\partial \sigma_{xy}}{\partial y}$

Volume flux:  $Q = \beta^{-\frac{1}{n}} \frac{n}{2n+1} \left( \rho g - \frac{dp}{dx} \right)^{\frac{1}{n}} h^{(2+\frac{1}{n})}$

Note:  $(\cdot)^{\frac{1}{n}} = \text{sign}(\cdot) \cdot |\cdot|^{\frac{1}{n}}$

Mass conservation:  $h_t + Q_x = 0$

# Governing equations

## Non-dimensionalisation

Lengthscales:

- ▶ Fibre radius,  $a$ , in  $x$  direction.
- ▶ Initial film thickness,  $h_0$ , in  $y$  direction.

Time:

- ▶ Rayleigh instability,  $\frac{2n+1}{n} \left( \frac{\beta a^{n+3}}{\gamma h_0^{n+2}} \right)^{\frac{1}{n}}$ .

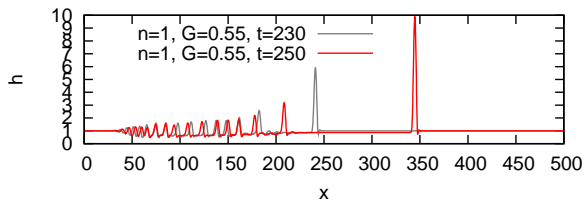
$$h_t + \left( h^{2+\frac{1}{n}} (G + (h + h_{xx})_x)^{\frac{1}{n}} \right)_x = 0$$

where Bond number  $G = \frac{\rho g a^3}{\gamma h_0}$ .

# Time-dependent numerical simulations

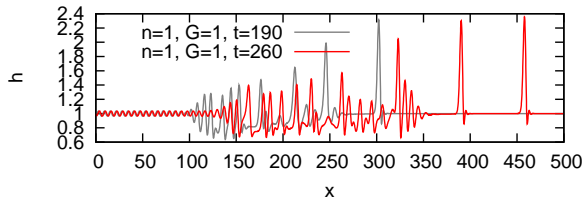
Periodic forcing at inlet:  $\omega = 1$

**G** small (thicker film):



Ever growing  
large pulses

**G** big (thinner film):



Solitary waves  
of similar  
amplitude and  
speed

This talk: Solitary waves? When? Properties?

# Stationary solitary waves

## Governing equations

In the frame of the solitary waves travelling with speed  $c$ :

$$(G + (h + h_{xx})_x) = \frac{\left(c(h - 1) + G\frac{1}{n}\right)^n}{h^{2n+1}}$$

$$h \rightarrow 1, \quad \text{as } x \rightarrow \pm\infty$$

Numerically construct the stationary solitary waves.

- ▶ Integrate from  $x = -\infty$  to  $x = 0$ ,  
and from  $x = +\infty$  to  $x = 0$ .
- ▶ Hence need starting conditions at  $x = \pm\infty$ .



# Stationary solitary waves

Initial conditions for numerics

At  $x = \pm\infty$ :  $h \sim 1 + \tilde{h}$  with  $\tilde{h} \ll 1$ .

Linearised equation:

$$\tilde{h}''' + \tilde{h}' - A\tilde{h} = 0$$

where  $A = nG^{1-1/n}c - (2n+1)G > 0$ .

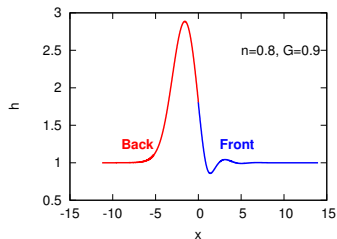
Three solutions of exponential form:

- ▶  $\tilde{h}_1 = a_1 e^{m_1 x}$   
 $m_1$  real and positive: growing mode.

Use in 'Back' (1 DoF).

- ▶  $\tilde{h}_{2,3} = a_{2,3} e^{m_{2,3} x}$   
 $m_{2,3}$  complex conjugates with negative real part: decaying modes.

Use in 'Front' (2 DoF).

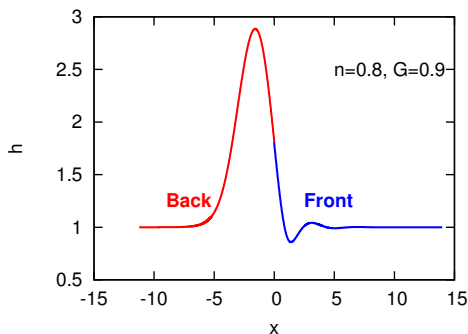


# Stationary solitary waves

## Numerical construction

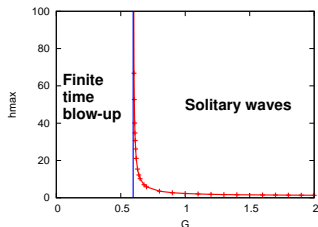
For fixed  $G$ :

1. Shoot from **Back**, with  $a_2 = a_3 = 0$ . Stop when  $h'' = 0$ ,  $h' < 0$ .
2. Shoot from **Front**, with  $a_1 = 0$ . Stop when  $h'' = 0$ ,  $h' < 0$ ,  $h > 1.5$ .
3. Vary the phase of  $a_{2,3}$  in **Front** to match  $h$ .
4. Vary speed  $c$  to match  $h'$ .

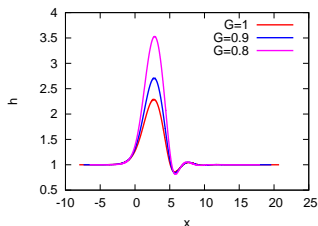


# Stationary solitary waves

Results:  $n = 1$  Kalliadasis & Chang, J. Fluid Mech. 1994



- ▶ No stationary solitary waves for  $G < G_0$ .
- ▶ As  $G \downarrow G_0+$ ,  $h_{\max} \rightarrow \infty$ .



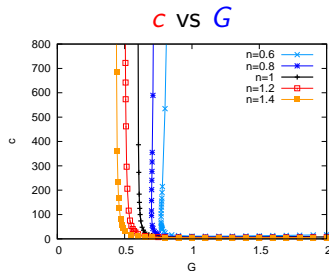
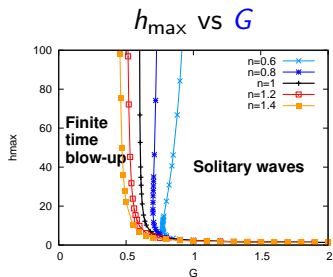
- ▶ Width of the 'Main Body' independent of  $G$ .

Agreement with experiment Quéré, Europhys. Lett. 1990:

- ▶ Critical  $h_c$  to observe disturbance  $\propto a^3$ .
- ▶  $G = \frac{\rho g a^3}{\sigma h_0} \Rightarrow h_c \propto a^3$  at  $G = G_0$ .

# Stationary solitary waves

Results: various  $n$  (shear-thinning and shear-thickening)



- ▶ Two branches of solutions for  $n < 1$ .

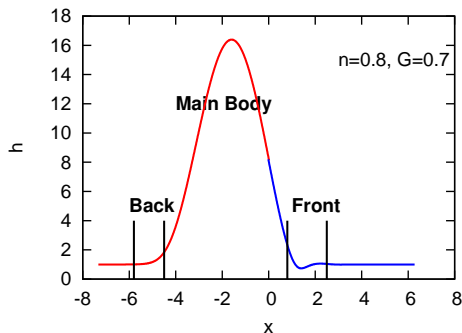
Look at large fast stationary solitary waves close to  $G_0$ .

What determines critical  $G_0$ ? Relationship of  $h$  and  $c$  with  $G$ ?

# Large fast solitary waves

Pulse divided into 3 regions:

- ▶ 'Main body' region:  $h$  big,  $x \sim O(1)$ .
- ▶ 'Front' and 'Back' transition regions:  $h \sim O(1)$ ,  $x$  small.



Asymptotic analysis for each region, and match. **Very complicated!**

# Large fast solitary waves

Main body region: leading order

$h$  big,  $x \sim O(1)$

$$(G + (\mathbf{h} + \mathbf{h}_{xx})_x) = \frac{(c(h-1) + G^{\frac{1}{n}})^n}{h^{2n+1}}$$

Solution: constant capillary pressure ( $p = \frac{1}{2}h_{\max}$ )

$$h = \frac{1}{2}h_{\max}(1 - \cos x) \quad \text{in} \quad 0 \leq x \leq 2\pi.$$

For matching,

$$h \sim \frac{1}{4}h_{\max}(x - x_0)^2,$$

with  $x_0 = 0$  at the Back and  $x_0 = 2\pi$  at the Front.

At leading order main body is at a constant pressure

# Large fast solitary waves

Transition regions: leading order

$h \sim O(1)$ ,  $x$  small

$$(G + (h + h_{xx})_x) = \frac{(c(h-1) + G^{\frac{1}{n}})^n}{h^{2n+1}}$$

Transition regions:  $x \sim c^{-n/3}$ .

Modified Bretherton equation:

$$h_{\xi\xi\xi} = \frac{(h-1)^n}{h^{2n+1}} \quad \text{with} \quad \xi = c^{n/3}(x - x_0).$$

( $x_0 = 0$  at 'Back' and  $x_0 = 2\pi$  at 'Front'.)

# Large fast solitary waves

Transition regions: leading order

$h \sim O(1)$ ,  $x$  small

$$(G + (h + \mathbf{h}_{xx})_x) = \frac{(c(\mathbf{h} - 1) + G^{\frac{1}{n}})^n}{\mathbf{h}^{2n+1}}$$

Transition regions:  $x \sim c^{-n/3}$ .

Modified Bretherton equation:

$$h_{\xi\xi\xi} = \frac{(h-1)^n}{h^{2n+1}} \quad \text{with} \quad \xi = c^{n/3}(x - x_0).$$

( $x_0 = 0$  at 'Back' and  $x_0 = 2\pi$  at 'Front'.)

For matching, solutions towards 'Main Body' ( $h$  becoming large)

$$h \sim \frac{1}{2}P_{\pm}\xi^2 + Q\xi + R_{\pm} \quad \text{as} \quad \xi \rightarrow \pm\infty$$

Use 1 DoF to redefine origin so  $Q = 0$ .



# Large fast solitary waves

Matching: leading order

DoFs at Back:  $1 - 1(Q = 0) = 0$ .  $P_+$  and  $R_+$  uniquely determined.

DoFs at Front:  $2 - 1(Q = 0) = 1$ . One parameter in  $P_-$  and  $R_-$ .

Main body:  $h \sim \frac{1}{4} h_{\max} (x - x_0)^2$  near  $x_0 = 0, 2\pi$ .

Transition regions:  $h \sim \frac{1}{2} P_{\pm} \xi^2 + R_{\pm}$  as  $\xi \rightarrow \pm\infty$ .

Matching:

$$P_- = P_+$$

So now  $P_-$  unique and hence  $R_-$  unique.

$$\frac{1}{2} P (\xi = c^{n/3} (x - x_0))^2 = \frac{1}{4} h_{\max} (x - x_0)^2$$

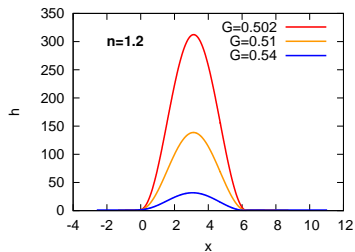
$$h_{\max} = 2P c^{2n/3}$$

Note: capillary pressure in the main body  $p = \frac{1}{2} h_{\max} = P c^{2n/3}$ .

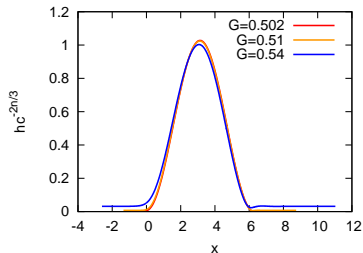
# Large fast solitary waves

## Checking scalings

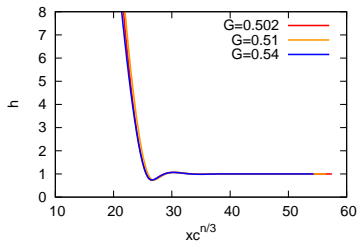
Original profile:



Main body:  
height scaled by  $c^{-2n/3}$



'Front' transition region:  
width scaled by  $c^{n/3}$



# Large fast solitary waves

So far have  $h_{\max}(c)$ .  $G$  yet to appear

Transition regions:  $h \sim \frac{1}{2}P\xi^2 + R_{\pm}$ .

- ▶ Different apparent film thickness,  $R_{\pm}$ , at 'Back' and 'Front'.

Need 1st correction of Main Body:  $h \sim c^{2n/3}h_0 + h_2$

$$(G + (h + h_{xx})_x) = \frac{(c(h-1) + G^{1/n})^n}{h^{2n+1}}$$

$$G_0 + (h_2 + h_{2xx})_x = 0$$

# Large fast solitary waves

So far have  $h_{\max}(c)$ .  $G$  yet to appear

Transition regions:  $h \sim \frac{1}{2}P\xi^2 + R_{\pm}$ .

- ▶ Different apparent film thickness,  $R_{\pm}$ , at 'Back' and 'Front'.

Need 1st correction of Main Body:  $h \sim c^{2n/3}h_0 + h_2$

$$(G + (h + h_{xx})_x) = \frac{(c(h-1) + G^{1/n})^n}{h^{2n+1}}$$

$$G_0 + (h_2 + h_{2xx})_x = 0$$

Solution (hydrostatic pressure gradient):

$$h_2 = -G_0(x - \sin x) + R_+ \quad \text{in } 0 \leq x \leq 2\pi.$$

Matching gives critical  $G_0$ :

$$G_0 = (R_+ - R_-)/2\pi$$

$2\pi G_0$  pressure difference between pushing and pulling transitions

# Large fast solitary waves

$c$  as a function of  $G$

So far have  $h_{\max}(c)$  and critical  $G_0$ . Yet to find  $G(c)$ .

Need 2nd correction:

$$h \sim c^{2n/3} h_0 + h_2 + c^{-(2n-1)n/3} h_3$$

$$G = G_0 + c^{-(2n-1)n/3} G_1$$

$$(h_3 + h_{3xx})_x = \left( \frac{1}{P^{n+1}(1 - \cos x)^{n+1}} - G_1 \right)$$

Solution

$$P^{n+1} h_3 = \frac{(n+1) \sin x}{n(2n+1)(1 - \cos x)^n} - \frac{(n + (n+1) \cos x) \sin x}{(2n+1)(2n-1)(1 - \cos x)^n} \\ + \frac{(n-1)(n + (n+1) \cos x)}{(2n+1)(2n-1)} + \int_{\pi}^x \frac{1}{(1 - \cos t)^{n-1}} dt - G_1 x$$

# Large fast solitary waves

$c$  as a function of  $G$

Near  $x = x_0$

$$h_3 \sim S(x - x_0)^{1-2n} + D_{\pm} - G_1 x + \dots$$

- ▶ The **singular term** matches the same in transition regions.
- ▶  $D_{\pm}$  different at the 'Back' and 'Front'.
- ▶ No terms to match with them from transition regions.
- ▶ Hence need:

$$G_1 = (D_+ - D_-)/2\pi$$

Finally we have found the relationship between  $c$  and  $G$

$$G = G_0 + c^{-(2n-1)n/3} G_1$$

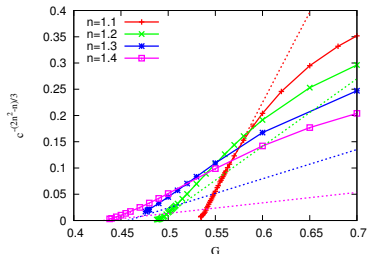
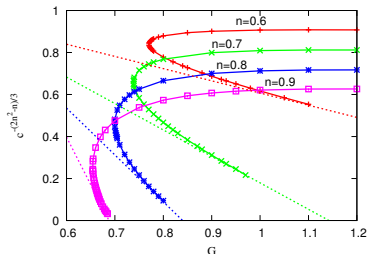
$2\pi G_1$  is the extra pressure difference to drive flow through main body compared with  $n = 1$

# Large fast solitary waves

## Results

$$G = G_0 + c^{-(2n-1)n/3} G_1$$

Plot  $c^{-(2n-1)n/3}$  vs  $G$



- ▶ When  $n < 1$ ,  $G_1 < 0$ . Negative slope at  $G_0$ .
- ▶ When  $n > 1$ ,  $G_1 > 0$ . Positive slope at  $G_0$ .
- ▶ When  $n = 1$ ,  $G_1 = 0$ . No relationship between  $G$  and  $c$  yet.

# More terms

transition regions

With scaling  $\xi = c^{n/3}(x - x_0)$ ,

$$h_{\xi\xi\xi} = \frac{(h-1)^n}{h^{2n+1}} - c^{-2n/3} h_{\xi} - c^{-n} G + c^{-1} \frac{n(h-1)^{n-1} G^{1/n}}{h^{2n+1}} + \dots$$

Expand  $h$  as

$$h \sim h_0 + c^{-2n/3} h_2 + c^{-n} h_3 + c^{-1} h_4 + c^{-4n/3} h_5 + \dots$$

$$h_0''' = \frac{(h-1)^n}{h^{2n+1}},$$

$$h_0 \sim \frac{P}{2} \xi^2 + R_{\pm} + Sx^{1-2n}$$

$$h_2''' = \frac{(h_0-1)^{n-1}(-(n+1)h_0 + (2n+1))}{h_0^{2n+2}} h_2 - h_0',$$

$$h_2 \sim -\frac{P}{4!} \xi^4 + \frac{a_{2\pm}}{2} \xi^2 + c_{2\pm} + k_2 \xi^{3-2n}$$

$$h_3''' = \frac{(h_0-1)^{n-1}(-(n+1)h_0 + (2n+1))}{h_0^{2n+2}} h_3 - G_0,$$

$$h_3 \sim -\frac{G_0}{3!} \xi^3 + \frac{a_{3\pm}}{2} \xi^2 + c_{3\pm}$$

$$h_4''' = \frac{(h_0-1)^{n-1}(-(n+1)h_0 + (2n+1))}{h_0^{2n+2}} h_4$$

$$h_4 \sim \frac{1}{2} a_{4\pm} \xi^2 + c_{4\pm}$$

$$+ \frac{n(h_0-1)^{n-1} G_0^{1/n}}{h_0^{2n+1}},$$



# More terms

main body

With  $h = c^{2n/3}H$ ,

$$(H + H_{xx})_x = -c^{-2n/3}G + c^{-(2n+1)n/3} \frac{\left(1 - \frac{c^{-2n/3}}{H} + \frac{G^{1/n}(c^{-1-2n/3})}{H}\right)^n}{H^{n+1}}.$$

Expand  $H$  as

$$H \sim H_0 + c^{-2n/3}H_2 + c^{-(2n+1)n/3}H_3 + c^{-n}H_4 + c^{-1}H_5 + c^{-4n/3}H_6 + \dots$$

and  $G$  as

$$G \sim G_0 + G_1c^{-(2n-1)n/3} + G_2c^{-2n/3} + \dots$$

$$H'_0 + H''_0 = 0,$$

$$H'_2 + H''_2 = -G_0$$

$$H'_3 + H''_3 = -G_1 + \frac{1}{P^{n+1}(1 - \cos x)^{n+1}},$$

$$H'_4 + H''_4 = 0,$$

$$H'_5 + H''_5 = 0,$$

$$H'_6 + H''_6 = -G_2,$$

$$H_0 = P(1 - \cos x)$$

$$H_2 = G_0(\sin x - x) + A_2 + C_2 \cos x$$

$$H_3 \sim Sx^{1-2n} + D_{\pm} - G_1x + k_2x^{3-2n}$$

$$H_4 = A_4 + B_4 \sin x + C_4 \cos x$$

$$H_5 = A_5 + B_5 \sin x + C_5 \cos x$$

$$H_6 = G_2(\sin x - x) + A_6 + B_6 \sin x + C_6 \cos x$$

# More terms

Matching: transition regions

Transition regions=

	$h_0$	$h_2$	$h_3$	$h_4$	$h_5$	
$c^{\frac{2n}{3}}$	$\left[ \frac{P}{2}x^2 \right.$	$\left. -\frac{P}{4!}x^4 \right.$			$\left. +\frac{P}{6!}x^6 \right.$	$\left. + \dots \right]$
$+c^0$	$\left[ R_{\pm} \right.$	$\left. +\frac{a_2}{2}x^2 \right.$	$\left. -\frac{G_0}{3!}x^3 \right.$		$\left. -\frac{a_2}{4!}x^4 \right.$	$\left. + \dots \right]$
$+c^{-\frac{2n^2}{3}+\frac{n}{3}}$	$\left[ Sx^{1-2n} \right.$	$\left. +k_2x^{3-2n} \right.$			$\left. +k_3x^{5-2n} \right.$	$\left. + \dots \right]$
$+c^{-\frac{n}{3}}$	$\left[ \right.$		$\left. +\frac{a_3}{2}x^2 \right.$			$\left. + \dots \right]$
$+c^{\frac{2n}{3}-1}$	$\left[ \right.$			$\left. \frac{a_4}{2}x^2 \right.$		$\left. + \dots \right]$
$+c^{-\frac{2n}{3}}$	$\left[ \right.$	$\left. C_{2\pm} \right.$			$\left. +\frac{a_5}{2}x^2 \right.$	$\left. + \dots \right]$

# More terms

Matching: main body region

Main body=

$$\begin{aligned} & c^{\frac{2n}{3}} \left[ \frac{P}{2}x^2 - \frac{P}{4!}x^4 + \frac{P}{6!}x^6 + \dots \right] \\ & + c^0 \left[ -G_0x_0 + A_2 + C_2 - \frac{C_2}{2}x^2 - \frac{G_0}{3!}x^3 + \frac{C_2}{4!}x^4 + \dots \right] \\ & + c^{-\frac{2n^2}{3} + \frac{n}{3}} \left[ Sx^{1-2n} - G_1x_0 + D_{\pm} + k_2x^{3-2n} + k_3x^{5-2n} + \dots \right] \\ & + c^{-\frac{n}{3}} \left[ A_4 + C_4 - \frac{C_4}{2}x^2 + \dots \right] \\ & + c^{\frac{2n}{3}-1} \left[ A_5 + C_5 - \frac{C_5}{2}x^2 \right] \\ & + c^{-\frac{2n}{3}} \left[ -G_2x_0 + A_6 + C_6 - \frac{C_6}{2}x^2 - \frac{G_2+B_6}{3!}x^3 + \dots \right] \end{aligned}$$

## More terms: matching two regions

At  $c^0$ :

$$G_0 = (R_+ - R_-)/2\pi$$

At  $c^{-(2n^2-n)/3}$ :

$$G_1 = -(D_+ - D_-)/2\pi$$

At  $c^{-1}$ :

$$G_2 = (c_{2+} - c_{2-})/2\pi$$

Hence,

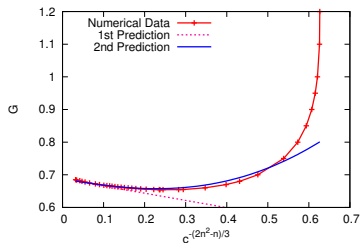
$$G = G_0 + G_1 c^{-(2n-1)n/3} + G_2 c^{-2n/3}$$

# More terms: Results

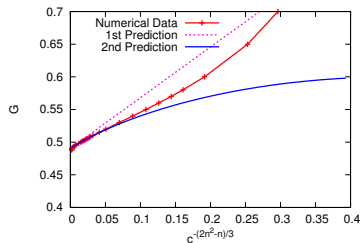
$$G = G_0 + G_1 c^{-(2n-1)n/3} + G_2 c^{-2n/3}$$

Plot  $G$  vs  $c^{-(2n-1)n/3}$

$n = 0.9$



$n = 1.2$



## More terms: Results

$$G = G_0 + G_1 c^{-(2n^2-n)/3} + G_2 c^{-2n/3}$$

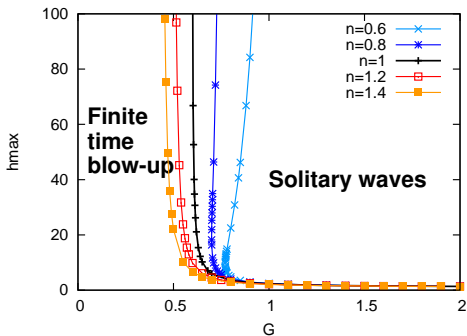
When  $n = 1$ ,  $G_1 = 0$ , so

$$G = G_0 + G_2 c^{-2/3}$$

Need even more terms for Newtonian  $n = 1$  – see beyond end.

$2\pi G_2$  comes from corrections in the transition regions due to the small axial curvature

# Two branches for $n < 1$



Upper branch is unstable – solutions either blow up or decay to lower branch.

Hence there is a maximum size of stable solitary for shear-thinning fluids.

# Future Work

- ▶ Normal stress effect. ✓
- ▶ Relax the thin film approximation? ✓  
    A third mechanism to determine  $G(c)$
- ▶ Newtonian fluid  $n = 1$  ✓
- ▶ What happens at big  $G$ ? ✓
- ▶ Finite flow domain for shear-thinning fluids ✓
- ▶ Comparison with experimental data.





# Symmetry breaking instability with elastic liquids

with Claire McIlroy

- ▶ François Boulogne observed in his Paris PhD thesis that the coating of an elastic liquid was never axisymmetric, but was always thicker on one side.
- ▶ Flow in thin coating is mainly simple shear and quasi-steady (varies over distances much greater than thickness).
- ▶ Hence rheology is a viscosity plus normal stresses.
- ▶ First normal stress difference = tension in streamlines → enhanced effective surface tension.
- ▶ Second normal stress difference = tension in vortex lines → new instability.

# Symmetry breaking instability with elastic liquids

Governing equation

Extra non-Newtonian stress for a second-order fluid

$$\sigma^{NN} = -2\alpha \overset{\nabla}{E} + \beta E^2,$$

$\alpha$  tension in the streamlines,  $\beta < 0$  tension in the vortex lines.

$$\frac{\partial h}{\partial t} + \frac{\partial h}{\partial z} - \nabla h^3 \nabla \nabla^2 h - A \frac{\partial^2}{\partial z^2} h^5 - B \frac{\partial^2}{\partial \theta^2} h^5 = 0,$$

(curiously  $A \sim \alpha/6$ , but  $B \sim -\beta/80$ )

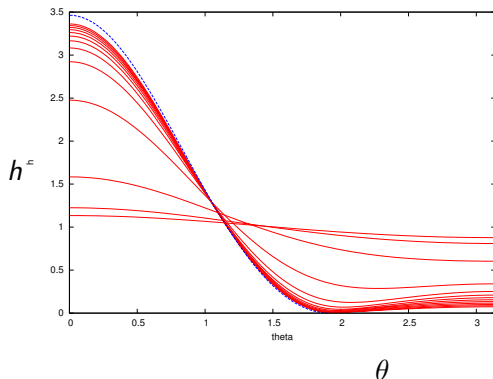
Now study development of lop-sided flow with  $h(\theta, t)$ , no  $z$ -variations.

$$h_t - (h^3(h_{\theta\theta} + h + Bh^2))_{\theta} = 0$$

# Symmetry breaking instability with elastic liquids

Time evolution

$h(\theta, t)$  at  $t = 2^n$   $n = -2, \dots, 11$ , for  $B = 0.5$ .



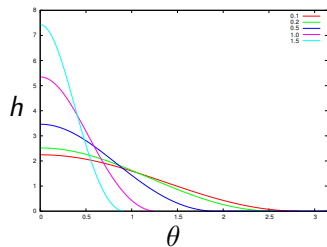
Dotted blue is a steady state which wets only  $0 \leq \theta \leq 1.9071$

(Interesting intermediate times: drift of an off-centred cylinder.)

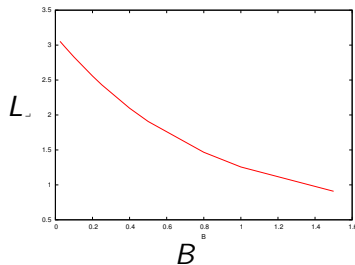
# Symmetry breaking instability with elastic liquids

## Steady states

Steady states for various  $B$



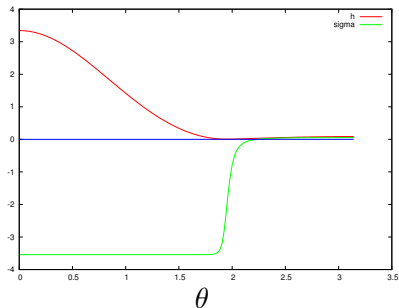
Length of steady state



# Symmetry breaking instability with elastic liquids

## Structure of steady states

The shape and the pressure (stress  $\sigma_{\theta\theta}$ ) at  $t = 10^3$  for  $B = 0.5$



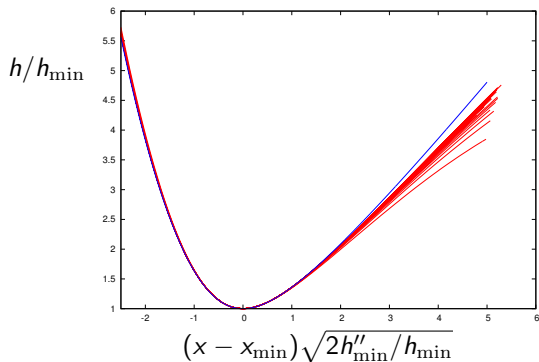
There two constant pressure regions.

The higher pressure region to the right is draining into the lower pressure region to the left through a small neck.

# Symmetry breaking instability with elastic liquids

The neck between the two constant pressure regions

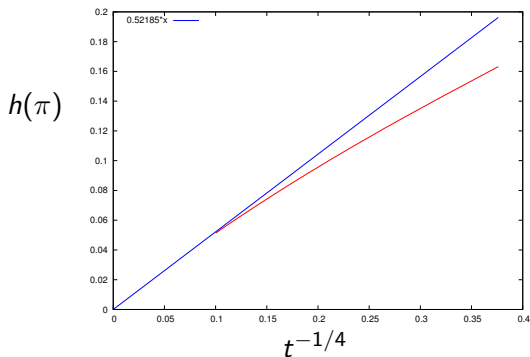
Universal shape of the neck between the two constant pressure regions, for  $t = 50$  ( $50 \cdot 10^3$ ) and for  $B = 0.5$ .



Blue shape from Bretherton's equation.

# Symmetry breaking instability with elastic liquids

Draining of small region



$$h(\pi) = \frac{1 + \cos L}{t^{1/4}} \left( \frac{K((\pi - L) \cos L + \sin L)}{4Q \sin^5 L} \right)^{1/4}$$

with Bretherton  $Q = 1.20936$  and for  $B = 0.5$  pressure in steady state lobe  $K = 3.7297$  and length of steady state lobe  $L = 1.9171$ .



# Future Work

- ▶ Normal stress effect. ✓
- ▶ Relax the thin film approximation? ✓
  - A third mechanism to determine  $G(c)$
- ▶ Newtonian fluid  $n = 1$  ✓
- ▶ What happens at big  $G$ ? ✓
- ▶ Finite flow domain for shear-thinning fluids ✓
- ▶ Comparison with experimental data.



# $n = 1$ Newtonian fluid, even more terms

Matching: transition regions

Transition regions=

	$h_0$	$h_2$	$h_3$	$h_4$	
$c^{2/3}$ [	$\frac{P}{2}x^2$	$-\frac{P}{4!}x^4$		$+\frac{P}{6!}x^6$	+ ... ]
+ $c^0$ [	$R_{\pm}$	$+\frac{a_2}{2}x^2$	$-\frac{G_0}{3!}x^3$	$-\frac{a_2}{4!}x^4$	+ ... ]
+ $c^{-1/3}$ [	$-\frac{2}{3P^2x}$		$+\frac{a_3}{2}x^2$	$+\frac{11}{1080P^2}x^3$	+ ... ]
+ $c^{-2/3}$ [		$+c_{2\pm}$		$+\frac{a_4}{2}x^2$	+ ... ]
+ $c^{-1} \log c$ [			$+\frac{4G_0}{9P^3}$		+ ... ]
+ $c^{-1}$ [	$\frac{2(1+2R_{\pm})}{15P^3x^3}$	$+\frac{8R_{\pm}+4+20a_2}{15P^3x}$	$+\frac{4G_0}{3P^3} \log x$	$+c_{3\pm}$	+ ... ]

# $n = 1$ Newtonian fluid, even more terms

Matching: main body region

Main body =

$$c^{2/3} \left[ \frac{P}{2}x^2 - \frac{P}{4!}x^4 + \frac{P}{6!}x^6 + \dots \right]$$

$$+c^0 \left[ -G_0x_0 + A_2 + C_2 - \frac{C_2}{2}x^2 - \frac{G_0}{3!}x^3 + \frac{C_2}{4!}x^4 + \dots \right]$$

$$+c^{-1/3} \left[ -\frac{2}{3P^2x} + (A_3 + C_3) + \left(\frac{1}{18P^2} + B_3\right)x - \frac{C_3}{2}x^2 + \left(\frac{1}{1080P^2} - \frac{B_3}{3!}\right)x^3 \dots \right]$$

$$+c^{-2/3} \left[ -G_2x_0 + A_4 + C_4 + B_4x - \frac{C_4}{2}x^2 - \frac{G_2}{3!}x^3 + \dots \right]$$

$$+c^{-1} \log c \left[ A_5 + C_5 - \frac{C_5}{2}x^2 + \dots \right]$$

$$+c^{-1} \left[ \frac{2(1+2R_{\pm})}{15P^3x^3} + \frac{4(1+2A_2-3C_2)}{15P^3x} + \frac{4G_0}{3P^3} \log x - G_3x_0 + A_6 + C_6 \dots \right]$$

# $n = 1$ Newtonian fluid, even more terms

## Results

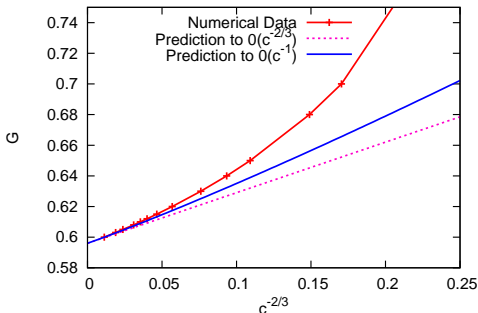
At  $c^0$ :  $G_0 = (R_+ - R_-)/2\pi$

At  $c^{-2/3}$ :  $G_2 = (c_{2+} - c_{2-})/2\pi$

At  $c^{-1}$ :  $G_3 = (c_{3+} - c_{3-})/2\pi$

Hence,

$$G = G_0 + G_2 c^{-2/3} + G_3 c^{-1}$$





$$h \sim 1 + \frac{1}{G} h_1 \quad c \sim \left(2 + \frac{1}{n}\right) G^{\frac{1}{n}} + c_1 G^{\frac{1}{n}-1}$$

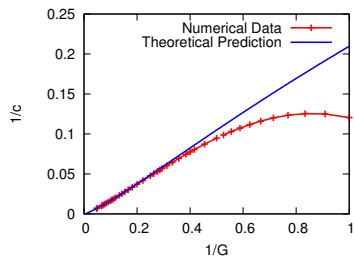
where  $h_1$  satisfies the nonlinear equation

$$h_1' + h_1''' = n c_1 h_1 + h_1^2 \left( -n(2n+1) + \frac{n(n-1)}{2} \left(2 + \frac{1}{n}\right)^2 \right)$$

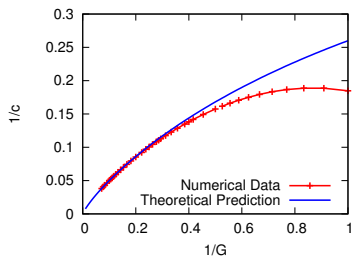
This equation can be solved numerically to give the value of  $c_1$  for different values of  $n$ .

# Big G results

$n = 0.8$



$n = 1.2$







# Finite flow domain for shear-thinning fluids

Modified Bretherton equation

$$h''' = \frac{(h-1)^n}{h^{2n+1}}$$

Integrating from  $\pm\infty$  where  $h \sim 1 + \tilde{h}$  ( $\tilde{h} \ll 1$ ),  $\tilde{h}$  satisfies:

$$\tilde{h}''' = \tilde{h}^n. \Leftarrow \text{No exponential solutions for } n \neq 1.$$

Solution at 'Back'

$$\tilde{h} = A(\xi - \xi_0)^{\frac{3}{1-n}}, \quad n < 1$$

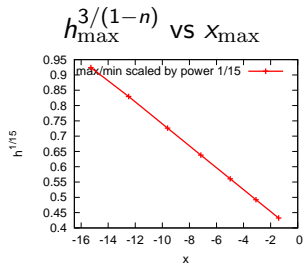
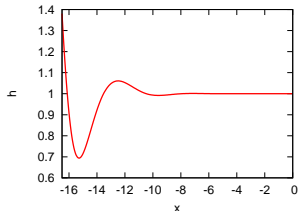
$\tilde{h}$  becomes 0 at a finite distance.

While viscosity thins as  $\gamma \rightarrow \infty$  it thickens as  $\gamma \rightarrow 0$ , and so flow stops in a finite distance.

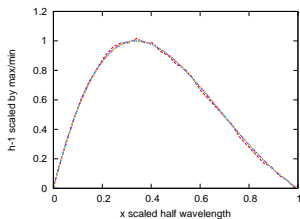
# Finite flow domain for shear-thinning fluids

Solution at 'Front' ( $n = 0.8$ )

## Decaying nonlinear oscillations



Each half-cycle normalised by maximum and by wavelength



Universal shape

Decays to zero in finite distance