To calculate the flow of complex fluids, need governing equations,

- To calculate the flow of complex fluids, need governing equations,
- in particular, the constitutive equation relating stress to flow and its history.

- To calculate the flow of complex fluids, need governing equations,
- in particular, the constitutive equation relating stress to flow and its history.
- Either 'ad hoc', such as Oldroyd-B differential equation and BKZ integral equation,

- To calculate the flow of complex fluids, need governing equations,
- in particular, the constitutive equation relating stress to flow and its history.
- Either 'ad hoc', such as Oldroyd-B differential equation and BKZ integral equation,
- Or look at microstructure for highly idealised systems and derive their constitutive equations.

- To calculate the flow of complex fluids, need governing equations,
- in particular, the constitutive equation relating stress to flow and its history.
- Either 'ad hoc', such as Oldroyd-B differential equation and BKZ integral equation,
- Or look at microstructure for highly idealised systems and derive their constitutive equations.
- Most will be suspensions of small particles in Newtonian viscous solvent.

## Microstructural studies for rheology

- Micro & macro views
- Einstein viscosity
- Rotations
- Deformations
- Interactions
- Polymers
- Others

# Micro & macro views

- Separation of length scales
- Micro  $\leftrightarrow$  Macro connections
- Case of Newtonian solvent
- Homogenisation

#### Essential

### Micro $\ell \ll L$ Macro

 $\mathsf{Micro} = \mathsf{particle} \ 1 \mu m \qquad \mathsf{Macro} = \mathsf{flow}, \ 1 cm$ 

#### Essential

# Micro $\ell \ll L$ Macro

 $Micro = particle 1 \mu m$  Macro = flow, 1 cm

Micro and Macro time scales similar

### Essential

### Micro $\ell \ll L$ Macro

 $\mathsf{Micro} = \mathsf{particle} \ 1 \mu m \qquad \mathsf{Macro} = \mathsf{flow}, \ 1 cm$ 

- Micro and Macro time scales similar
- ► Need  $\ell$  small for small micro-Reynolds number  $Re_{\ell} = \frac{\rho\gamma\ell^2}{\mu} \ll 1$ ,

### Essential

### Micro $\ell \ll L$ Macro

 $\mathsf{Micro} = \mathsf{particle} \ 1 \mu m \qquad \mathsf{Macro} = \mathsf{flow}, \ 1 cm$ 

- Micro and Macro time scales similar
- Need ℓ small for small micro-Reynolds number Re<sub>ℓ</sub> = <sup>ργℓ<sup>2</sup></sup>/<sub>μ</sub> ≪ 1, otherwise possible macro-flow boundary layers ≪ ℓ

### Essential

### Micro $\ell \ll L$ Macro

Micro = particle  $1\mu m$  Macro = flow, 1cm

- Micro and Macro time scales similar
- ► Need  $\ell$  small for small micro-Reynolds number  $Re_{\ell} = \frac{\rho \gamma \ell^2}{\mu} \ll 1$ , otherwise possible macro-flow boundary layers  $\ll \ell$ But macro-Reynolds number  $Re_L = \frac{\rho \gamma L^2}{\mu}$  can be large

### Essential

### Micro $\ell \ll L$ Macro

Micro = particle  $1\mu m$  Macro = flow, 1cm

- Micro and Macro time scales similar
- ► Need  $\ell$  small for small micro-Reynolds number  $Re_{\ell} = \frac{\rho\gamma\ell^2}{\mu} \ll 1$ , otherwise possible macro-flow boundary layers  $\ll \ell$ But macro-Reynolds number  $Re_L = \frac{\rho\gamma L^2}{\mu}$  can be large
- If  $\ell \not< L$ , then non-local rheology

Solve microstructure – tough, must idealise

- Solve microstructure tough, must idealise
- Extract macro-observables easy

- Solve microstructure tough, must idealise
- Extract macro-observables easy

Here: suspension of particles in Newtonian viscous solvent

Particles passively move with macro-flow u

- Particles passively move with macro-flow u
- ► Particles actively rotate, deform & interact with

macro-shear  $\nabla \mathbf{u}$ 

- Particles passively move with macro-flow u
- ▶ Particles actively rotate, deform & interact with

macro-shear  $\nabla \mathbf{u}$ 

both needing  $Re_{\ell} \ll 1$ .

Macro = continuum = average/smear-out micro details

Macro = continuum = average/smear-out micro details

E.g. average over representative volume V with  $\ell \ll V^{1/3} \ll L$ 

$$\overline{\sigma} = \frac{1}{V} \int_{V} \sigma \, dV$$

Macro = continuum = average/smear-out micro details

E.g. average over representative volume V with  $\ell \ll V^{1/3} \ll L$ 

$$\overline{\sigma} = \frac{1}{V} \int_{V} \sigma \, dV$$

Also ensemble averaging and homogenisation

Macro = continuum = average/smear-out micro details

E.g. average over representative volume V with  $\ell \ll V^{1/3} \ll L$ 

$$\overline{\sigma} = rac{1}{V} \int_V \sigma \, dV$$

Also ensemble averaging and homogenisation

To be used in averaged = macro momentum equation

$$\overline{\rho}\left[\frac{\partial \overline{\mathbf{u}}}{\partial t} + \overline{\mathbf{u}} \cdot \nabla \overline{\mathbf{u}}\right] = \nabla \cdot \overline{\sigma} + \overline{F}$$

Macro = continuum = average/smear-out micro details

E.g. average over representative volume V with  $\ell \ll V^{1/3} \ll L$ 

$$\overline{\sigma} = rac{1}{V} \int_V \sigma \, dV$$

Also ensemble averaging and homogenisation

To be used in averaged = macro momentum equation

$$\overline{\rho}\left[\frac{\partial \overline{\mathbf{u}}}{\partial t} + \overline{\mathbf{u}} \cdot \nabla \overline{\mathbf{u}}\right] = \nabla \cdot \overline{\sigma} + \overline{F}$$

NB micro-Reynolds stresses  $\overline{(\rho \mathbf{u})'\mathbf{u}'}$  small for  $Re_{\ell} \ll 1$ .

Write:

$$\sigma = -\boldsymbol{p}\boldsymbol{l} + 2\mu\boldsymbol{e} + \boldsymbol{\sigma}^+$$

with pressure p, solvent viscosity  $\mu$ , strain-rate e, and  $\sigma^+$  non-zero only inside particles.

Write:

$$\sigma = -pI + 2\mu e + \sigma^+$$

with pressure p, solvent viscosity  $\mu$ , strain-rate e, and  $\sigma^+$  non-zero only inside particles.

Average:

$$\overline{\sigma} = -\overline{p}I + 2\mu\overline{e} + \overline{\sigma^+}$$

Write:

$$\sigma = -pI + 2\mu e + \sigma^+$$

with pressure p, solvent viscosity  $\mu$ , strain-rate e, and  $\sigma^+$  non-zero only inside particles.

#### Average:

$$\overline{\sigma} = -\overline{p}I + 2\mu\overline{e} + \overline{\sigma^+}$$

with

$$\overline{\sigma^+} = rac{1}{V} \int_V \sigma^+ dV = n \left\langle \int_{\text{particle}} \sigma^+ dV \right\rangle_{\text{types of particle}}$$

with n number of particles per unit volume

Inside rigid particles e = 0, so  $\sigma^+ = \sigma$ .

Inside rigid particles e = 0, so  $\sigma^+ = \sigma$ .

Also  $\sigma_{ij} = \partial_k(\sigma_{ik}x_j) - x_j\partial_k\sigma_{ik}$ ,

Inside rigid particles e = 0, so  $\sigma^+ = \sigma$ .

Also  $\sigma_{ij} = \partial_k (\sigma_{ik} x_j) - x_j \partial_k \sigma_{ik}$ , ignoring gravity  $\partial_k \sigma_{ik} = 0$ ,

Inside rigid particles e = 0, so  $\sigma^+ = \sigma$ .

Also  $\sigma_{ij} = \partial_k (\sigma_{ik} x_j) - x_j \partial_k \sigma_{ik}$ , ignoring gravity  $\partial_k \sigma_{ik} = 0$ , so  $\int_{\text{particle}} \sigma^+ dV = \int_{\text{particle}} \sigma \cdot n \times dA$ 

Inside rigid particles e = 0, so  $\sigma^+ = \sigma$ .

Also 
$$\sigma_{ij} = \partial_k (\sigma_{ik} x_j) - x_j \partial_k \sigma_{ik}$$
, ignoring gravity  $\partial_k \sigma_{ik} = 0$ ,  
so  
$$\int_{\text{particle}} \sigma^+ dV = \int_{\text{particle}} \sigma \cdot n \times dA$$

so only need  $\sigma$  on surface of particle. (Detailed cases soon.)

Inside rigid particles e = 0, so  $\sigma^+ = \sigma$ .

Also 
$$\sigma_{ij} = \partial_k (\sigma_{ik} x_j) - x_j \partial_k \sigma_{ik}$$
, ignoring gravity  $\partial_k \sigma_{ik} = 0$ ,  
so  
$$\int_{\text{particle}} \sigma^+ dV = \int_{\text{particle}} \sigma \cdot n \times dA$$

so only need  $\sigma$  on surface of particle. (Detailed cases soon.)

Hence

$$\overline{\sigma} = -\overline{\rho}I + 2\mu\overline{e} + n\int_{\text{particle}} \sigma \cdot n \, x \, dA$$

Inside rigid particles e = 0, so  $\sigma^+ = \sigma$ .

Also 
$$\sigma_{ij} = \partial_k (\sigma_{ik} x_j) - x_j \partial_k \sigma_{ik}$$
, ignoring gravity  $\partial_k \sigma_{ik} = 0$ ,  
so  
 $\int_{\text{particle}} \sigma^+ dV = \int_{\text{particle}} \sigma \cdot n \times dA$ 

so only need  $\sigma$  on surface of particle. (Detailed cases soon.)

Hence

$$\overline{\sigma} = -\overline{p}I + 2\mu\overline{e} + n \int_{\text{particle}} \sigma \cdot n \, x \, dA$$

Integral called 'stresslet', is the force-dipole strength of the particle.

# Homogenisation: asymptotics for $\ell \ll L$
Easier transport problem to exhibit method

$$abla \cdot k \cdot 
abla T = Q$$

with k & Q varying on macroscale x and microscale  $\xi = x/\epsilon$ ,

Easier transport problem to exhibit method

$$abla \cdot k \cdot 
abla T = Q$$

with k & Q varying on macroscale x and microscale  $\xi = x/\epsilon$ ,

Multiscale asymptotic expansion

$$T(x;\epsilon) \sim T_0(x,\xi) + \epsilon T_1(x,\xi) + \epsilon^2 T_2(x,\xi)$$



 $\partial_{\xi} k \partial_{\xi} T_0 = 0$ 



$$\partial_{\xi} k \partial_{\xi} T_0 = 0$$

i.e. 
$$T_0 = T(x)$$

 $\epsilon^{-2}$ :

$$\partial_{\xi} k \partial_{\xi} T_0 = 0$$

i.e. 
$$T_0 = T(x)$$

Thus T varies only slowly at leading order, with microscale making small perturbations.



 $\partial_{\xi} k \partial_{\xi} T_1 = -\partial_{\xi} k \partial_x T_0$ 

 $\epsilon^{-1}$ :

$$\partial_{\xi} k \partial_{\xi} T_1 = -\partial_{\xi} k \partial_x T_0$$

Solution  $T_1$  is linear in forcing  $\partial_x T_0$ , details depending on  $k(\xi)$ :

 $\epsilon^{-1}$ :

$$\partial_{\xi} k \partial_{\xi} T_1 = -\partial_{\xi} k \partial_x T_0$$

Solution  $T_1$  is linear in forcing  $\partial_x T_0$ , details depending on  $k(\xi)$ :

 $T_1(x,\xi) = A(\xi)\partial_x T_0$ 

 $\epsilon^0$ :

#### $\partial_{\xi} k \partial_{\xi} T_{2} = Q - \partial_{x} k \partial_{x} T_{0} - \partial_{\xi} k \partial_{x} T_{1} - \partial_{x} k \partial_{\xi} T_{1}$

 $\epsilon^0$ :

$$\partial_{\xi} k \partial_{\xi} T_{2} = Q - \partial_{x} k \partial_{x} T_{0} - \partial_{\xi} k \partial_{x} T_{1} - \partial_{x} k \partial_{\xi} T_{1}$$

Secularity:  $\langle RHS \rangle = 0$  else  $T_2 = O(\xi^2)$  which contradicts asymptoticity. (Periodicity not necessary.)

$$\epsilon^0$$
:

$$\partial_{\xi} k \partial_{\xi} T_{2} = Q - \partial_{x} k \partial_{x} T_{0} - \partial_{\xi} k \partial_{x} T_{1} - \partial_{x} k \partial_{\xi} T_{1}$$

Secularity:  $\langle RHS \rangle = 0$  else  $T_2 = O(\xi^2)$  which contradicts asymptoticity. (Periodicity not necessary.) Hence

$$0 = \langle Q \rangle - \partial_x \langle k \rangle \partial_x T_0 - \partial_x \langle k \frac{\partial A}{\partial \xi} \rangle \partial_x T_0$$

$$\epsilon^{0}$$

$$\partial_{\xi} k \partial_{\xi} T_2 = Q - \partial_x k \partial_x T_0 - \partial_{\xi} k \partial_x T_1 - \partial_x k \partial_{\xi} T_1$$

Secularity:  $\langle RHS \rangle = 0$  else  $T_2 = O(\xi^2)$  which contradicts asymptoticity. (Periodicity not necessary.) Hence

$$0 = \langle Q \rangle - \partial_x \langle k \rangle \partial_x T_0 - \partial_x \langle k \frac{\partial A}{\partial \xi} \rangle \partial_x T_0$$

Hence macro description

$$abla k^* 
abla T = Q^*$$
 with  $k^* = \left\langle k + k rac{\partial A}{\partial \xi} 
ight
angle$  and  $Q^* = \langle Q 
angle$ 

NB: Leading order  $T_0$  uniform at microlevel, with therefore no local heat transport

NB: Leading order  $T_0$  uniform at microlevel, with therefore no local heat transport

NB: Micro problem forced by  $\nabla T_0$ . Need to solve

 $abla \cdot k 
abla \cdot T_{
m micro} = 0$   $T_{
m micro} o x \cdot 
abla T_0$ 

NB: Leading order  $T_0$  uniform at microlevel, with therefore no local heat transport

NB: Micro problem forced by  $\nabla T_0$ . Need to solve

 $abla \cdot k 
abla \cdot T_{
m micro} = 0$   $T_{
m micro} o x \cdot 
abla T_0$ 

Solution

$$T_{\rm micro} = (x + \epsilon A) \nabla T_0$$

NB: Leading order  $T_0$  uniform at microlevel, with therefore no local heat transport

NB: Micro problem forced by  $\nabla T_0$ . Need to solve

 $abla \cdot k 
abla \cdot T_{
m micro} = 0$   $T_{
m micro} o x \cdot 
abla T_0$ 

Solution

$$T_{\text{micro}} = (x + \epsilon A) \nabla T_0$$

Hence heat flux

$$\langle q \rangle = \langle k \nabla T_{\text{micro}} \rangle = \langle k + \epsilon k \nabla A \rangle \nabla T_0$$

## Micro & macro views

- Separation of length scales
- Micro  $\leftrightarrow$  Macro connections
- Case of Newtonian solvent
- Homogenisation

## Microstructural studies for rheology

- Micro & macro views
- Einstein viscosity
- Rotations
- Deformations
- Interactions
- Polymers
- Others

## Einstein viscosity

## Einstein viscosity

Simplest - can show all details.

Highly idealised - many generalisations

Highly idealised - many generalisations

Spheres – no orientation problems

Highly idealised – many generalisations

- Spheres no orientation problems
- Rigid no deformation problems

Highly idealised – many generalisations

- Spheres no orientation problems
- Rigid no deformation problems
- Dilute and Inert no interactions problems

Highly idealised – many generalisations

- Spheres no orientation problems
- Rigid no deformation problems
- Dilute and Inert no interactions problems

Highly idealised – many generalisations

- Spheres no orientation problems
- Rigid no deformation problems
- Dilute and Inert no interactions problems

#### Micro problem

Isolated rigid sphere

Highly idealised - many generalisations

- Spheres no orientation problems
- Rigid no deformation problems
- Dilute and Inert no interactions problems

- Isolated rigid sphere
- force-free and couple-free

Highly idealised - many generalisations

- Spheres no orientation problems
- Rigid no deformation problems
- Dilute and Inert no interactions problems

- Isolated rigid sphere
- force-free and couple-free
- in a general linear shearing flow  $\nabla \overline{U}$

Highly idealised - many generalisations

- Spheres no orientation problems
- Rigid no deformation problems
- Dilute and Inert no interactions problems

- Isolated rigid sphere
- force-free and couple-free
- in a general linear shearing flow  $\nabla \overline{U}$
- Stokes flow

$$abla \cdot \mathbf{u} = 0 \quad \text{in} \quad r > a$$
 $0 = -\nabla p + \mu \nabla^2 \mathbf{u} \quad \text{in} \quad r > a$ 

$$\nabla \cdot \mathbf{u} = 0 \quad \text{in} \quad r > a$$
$$0 = -\nabla p + \mu \nabla^2 \mathbf{u} \quad \text{in} \quad r > a$$

$$\begin{split} \mathbf{u} &= \mathbf{V} + \omega \times \mathbf{x} \quad \text{on} \quad r = \mathbf{a} \quad \text{with} \quad \mathbf{V}, \omega \text{ consts} \\ \mathbf{u} &\to \overline{U} + \mathbf{x} \cdot \nabla \overline{U} \quad \text{as} \quad r \to \infty \end{split}$$

$$\nabla \cdot \mathbf{u} = 0 \quad \text{in} \quad r > a$$
$$0 = -\nabla p + \mu \nabla^2 \mathbf{u} \quad \text{in} \quad r > a$$

$$\begin{split} \mathbf{u} &= \mathbf{V} + \omega \times \mathbf{x} \quad \text{on} \quad r = a \quad \text{with} \quad V, \omega \text{ consts} \\ \mathbf{u} &\to \overline{U} + \mathbf{x} \cdot \nabla \overline{U} \quad \text{as} \quad r \to \infty \end{split}$$

$$\mathbf{F} = \int_{r=a} \sigma \cdot n \, dA = 0, \qquad \mathbf{G} = \int_{r=a} \mathbf{x} \times \sigma \cdot n \, dA = 0$$

$$\nabla \cdot \mathbf{u} = 0 \quad \text{in} \quad r > a$$
$$0 = -\nabla p + \mu \nabla^2 \mathbf{u} \quad \text{in} \quad r > a$$

$$\begin{split} \mathbf{u} &= \mathbf{V} + \omega \times \mathbf{x} \quad \text{on} \quad r = \mathbf{a} \quad \text{with} \quad \mathbf{V}, \omega \text{ consts} \\ \mathbf{u} &\to \overline{U} + \mathbf{x} \cdot \nabla \overline{U} \quad \text{as} \quad r \to \infty \end{split}$$

$$\mathbf{F} = \int_{r=a} \sigma \cdot n \, dA = 0, \qquad \mathbf{G} = \int_{r=a} \mathbf{x} \times \sigma \cdot n \, dA = 0$$

Split general linear shearing flow  $\nabla \overline{U}$  into symmetric strain-rate **E** and antisymmetric vorticity  $\Omega$ , i.e.

$$\mathbf{x} \cdot \nabla \overline{U} = \mathbf{E} \cdot \mathbf{x} + \mathbf{\Omega} \times \mathbf{x}$$

$$\nabla \cdot \mathbf{u} = 0 \quad \text{in} \quad r > a$$
$$0 = -\nabla p + \mu \nabla^2 \mathbf{u} \quad \text{in} \quad r > a$$

$$\begin{split} \mathbf{u} &= \mathbf{V} + \boldsymbol{\omega} \times \mathbf{x} \quad \text{on} \quad r = \mathbf{a} \quad \text{with} \quad V, \boldsymbol{\omega} \text{ consts} \\ \mathbf{u} &\to \overline{U} + \mathbf{x} \cdot \nabla \overline{U} \quad \text{as} \quad r \to \infty \end{split}$$

$$\mathbf{F} = \int_{r=a} \sigma \cdot n \, dA = 0, \qquad \mathbf{G} = \int_{r=a} \mathbf{x} \times \sigma \cdot n \, dA = 0$$

Split general linear shearing flow  $\nabla \overline{U}$  into symmetric strain-rate **E** and antisymmetric vorticity  $\Omega$ , i.e.

$$\mathbf{x} \cdot \nabla \overline{U} = \mathbf{E} \cdot \mathbf{x} + \mathbf{\Omega} \times \mathbf{x}$$

NB: Stokes problem is linear and instantaneous Student Ex

### Solution of Stokes problem for Einstein viscosity

▶  $\mathbf{F} = 0$  gives  $\mathbf{V} = \overline{U}$ , i.e. translates with macro flow S.Ex

### Solution of Stokes problem for Einstein viscosity

- ▶  $\mathbf{F} = 0$  gives  $\mathbf{V} = \overline{U}$ , i.e. translates with macro flow S.Ex
- $\mathbf{G} = 0$  gives  $\omega = \Omega$ , i.e. rotates with macro flow S.Ex
### Solution of Stokes problem for Einstein viscosity

F = 0 gives V = U, i.e. translates with macro flow S.Ex
G = 0 gives ω = Ω, i.e. rotates with macro flow S.Ex
Then S.Ex

$$\mathbf{u} = \overline{U} + \mathbf{E} \cdot \mathbf{x} + \Omega \times \mathbf{x} - \mathbf{E} \cdot \mathbf{x} \frac{a^5}{r^5} - \mathbf{x} \frac{5(\mathbf{x} \cdot \mathbf{E} \cdot \mathbf{x})}{2r^2} \left(\frac{a^3}{r^3} - \frac{a^5}{r^5}\right)$$
$$p = -5\mu \frac{(\mathbf{x} \cdot \mathbf{E} \cdot \mathbf{x})a^3}{r^5}$$

### Solution of Stokes problem for Einstein viscosity

F = 0 gives V = U, i.e. translates with macro flow S.Ex
G = 0 gives ω = Ω, i.e. rotates with macro flow S.Ex
Then S.Ex

$$\mathbf{u} = \overline{U} + \mathbf{E} \cdot \mathbf{x} + \Omega \times \mathbf{x} - \mathbf{E} \cdot \mathbf{x} \frac{a^5}{r^5} - \mathbf{x} \frac{5(\mathbf{x} \cdot \mathbf{E} \cdot \mathbf{x})}{2r^2} \left(\frac{a^3}{r^3} - \frac{a^5}{r^5}\right)$$
$$p = -5\mu \frac{(\mathbf{x} \cdot \mathbf{E} \cdot \mathbf{x})a^3}{r^5}$$

Evaluate viscous stress on particle Student Ex

$$\sigma \cdot n \big|_{r=a} = \frac{5\mu}{2a} \mathbf{E} \cdot \mathbf{x}$$

### Solution of Stokes problem for Einstein viscosity

F = 0 gives V = U, i.e. translates with macro flow S.Ex
G = 0 gives ω = Ω, i.e. rotates with macro flow S.Ex
Then S.Ex

$$\mathbf{u} = \overline{U} + \mathbf{E} \cdot \mathbf{x} + \Omega \times \mathbf{x} - \mathbf{E} \cdot \mathbf{x} \frac{a^5}{r^5} - \mathbf{x} \frac{5(\mathbf{x} \cdot \mathbf{E} \cdot \mathbf{x})}{2r^2} \left(\frac{a^3}{r^3} - \frac{a^5}{r^5}\right)$$
$$p = -5\mu \frac{(\mathbf{x} \cdot \mathbf{E} \cdot \mathbf{x})a^3}{r^5}$$

Evaluate viscous stress on particle Student Ex

$$\sigma \cdot n \big|_{r=a} = \frac{5\mu}{2a} \mathbf{E} \cdot \mathbf{x}$$

Evaluate particle contribution to macro/average stress

$$\int_{\text{particle}} \sigma \cdot n \, \mathbf{x} \, dA = 5 \mu \mathbf{E} \frac{4\pi}{3} a^3$$

$$\overline{\sigma} = -\overline{
ho}I + 2\mu {f E} + 5\mu {f E} \phi$$
 with volume fraction  $\phi = n rac{4\pi}{3} a^3$ 

 $\overline{\sigma} = -\overline{\rho}I + 2\mu \mathbf{E} + 5\mu \mathbf{E}\phi$  with volume fraction  $\phi = n\frac{4\pi}{3}a^3$ 

$$\mu^* = \mu \left( 1 + \frac{5}{2} \phi \right)$$

 $\overline{\sigma} = -\overline{p}I + 2\mu \mathbf{E} + 5\mu \mathbf{E}\phi$  with volume fraction  $\phi = n\frac{4\pi}{3}a^3$ 

Hence effective viscosity

$$\mu^* = \mu \left( 1 + \frac{5}{2} \phi \right)$$

Result independent of type of flow – shear, extensional

 $\overline{\sigma} = -\overline{p}I + 2\mu \mathbf{E} + 5\mu \mathbf{E}\phi$  with volume fraction  $\phi = n\frac{4\pi}{3}a^3$ 

$$\mu^* = \mu \left( 1 + \frac{5}{2} \phi \right)$$

- Result independent of type of flow shear, extensional
- Result independent of particle size OK polydisperse

 $\overline{\sigma} = -\overline{p}I + 2\mu \mathbf{E} + 5\mu \mathbf{E}\phi$  with volume fraction  $\phi = n\frac{4\pi}{3}a^3$ 

$$\mu^* = \mu \left( 1 + \frac{5}{2} \phi \right)$$

- Result independent of type of flow shear, extensional
- Result independent of particle size OK polydisperse
- Einstein used another averaging of dissipation

 $\overline{\sigma} = -\overline{p}I + 2\mu \mathbf{E} + 5\mu \mathbf{E}\phi$  with volume fraction  $\phi = n\frac{4\pi}{3}a^3$ 

$$\mu^* = \mu \left( 1 + \frac{5}{2} \phi \right)$$

- Result independent of type of flow shear, extensional
- Result independent of particle size OK polydisperse
- Einstein used another averaging of dissipation which would not give normal stresses with σ : E = 0,

 $\overline{\sigma} = -\overline{p}I + 2\mu \mathbf{E} + 5\mu \mathbf{E}\phi$  with volume fraction  $\phi = n\frac{4\pi}{3}a^3$ 

$$\mu^* = \mu \left( 1 + \frac{5}{2} \phi \right)$$

- Result independent of type of flow shear, extensional
- Result independent of particle size OK polydisperse
- Einstein used another averaging of dissipation which would not give normal stresses with σ : E = 0, which arbitrarily cancelled divergent integrals (hydrodynamics is long-ranged)

# Microstructural studies for rheology

- Micro & macro views
- Einstein viscosity
- Rotations
- Deformations
- Interactions
- Polymers
- Others